

## Design of a Real-time Bubble Shape Detector for Gas-liquid Two-phase Flow in Coalbed Methane Development Wells Based on Optical Sensors

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### ABSTRACT

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#### Keywords:

*coalbed methane (CBM), gas-liquid two-phase flow, optical sensor, bubble velocity, bubble volume*

The coalbed methane (CBM) exists as a gas-liquid two-phase flow in the production well. However, the common bubble detector cannot identify bubbles in real time during the motion of the CBM gas-liquid two-phase flow. To solve the problem, this paper designs a real-time bubble shape detector for gas-liquid two-phase flow in CBM development wells using optical sensors. The detector design is based on the difference between gas and liquid in reflective index of light. With a STM32 processor, the light signals were converted to electricity signals, such that the light intensities are represented as electrical levels. The bubble velocity was calculated based on the distance between the probes of two sensors and the time for the bubble to pass through that distance. To obtain the bubble volume, the bubble diameter was firstly computed from the time the bubble takes to pass through the detection range of the sensor, and then coupled with the bubble velocity. The two time periods were determined by the high electrical levels outputted by sensor(s). Simulation shows that our detector measures the real-time bubble velocity and volume accurately under the CBM working conditions, while the traditional detectors can only identify the basic forms of bubble on the surface of media; moreover, our detector uses sapphire, a dampproof material, to mitigate the negative impact of humidity on detection accuracy. In addition, the probe does not react chemically with liquid, eliminating probe corrosion.

## 1. INTRODUCTION

Coalbed methane (CBM) is a form of natural gas extracted from coal beds. With methane as the main component, the CBM mainly exists in adsorbed form on coal matrix particles, partial free form within pores of coal beds, or dissolved form in the water of coal beds. To produce the CBM, wells are drilled into the coal beds, bringing groundwater to the surface. During discharge and decompression, gas-liquid two-phase flow is generated in the wellbore [1-5]. To effectively manage CBM production, it is necessary to monitor and control the gas-liquid two-phase flow of wellbore annulus [6]. The most direct way to determine the law of gas-liquid two-phase flow in CBM production wells lies in the real-time detection of bubble shape.

Many bubble detection devices have been developed for the gas-liquid two-phase flow in CBM production wells. For example, Wang et al. [7-12] designed a bubble detector based on light scattering imaging, which irradiates a laser beam into water, uses charge-coupled device (CCD) cameras to capture the lights scattered by bubbles, and processes the captured images on computer to obtain bubble speed, volume and local gas volume; the theoretical basis of the detector is that the laser beam can be scattered into lights of different intensities moving towards different directions, depending on the form of the bubbles. Zhang et al. [13-15] put forward a bubble detector based on the principle of ultrasonic attenuation: the ultrasonic signals attenuate differently after passing through different media. Considering ultrasound features and impedance difference between bubble and liquid, the detector

sends ultrasonic signals of a certain frequency and power from one side of a tank, receives the signals on the other side of the tank, and analyzes the signal attenuation on software to get bubble velocity and volume. The above two bubble detectors can identify the basic forms of bubble on the surface of media, but cannot detect bubble shape in the gas-liquid two-phase flow in CBM production. To solve the problem, Wu et al. [16-18] created a real-time CBM bubble detector in the light of the conductivity difference between gas and liquid; with this detector, the bubble shape can be determined accurately in real time by the obvious difference in conductivity between media. Nevertheless, the DC electrodes of the device are easily eroded by the liquid in the gas-liquid two-phase flow, and the conductive materials of the electrodes are often dampened, both of which lowers the accuracy of the detected results.

To overcome the defects of the existing bubble detectors, this paper proposes a real-time detector of CBM bubble shape using optical sensors. The detector design is based on the difference between gas and liquid in reflective index of light. After detailing the detection methods, the author verified the detector performance through a simulation of the gas-liquid two-phase flow in a CBM production well.

## 2. DESIGN PRINCIPLES

### 2.1 Theoretical basis

An optical sensor was designed based on the difference between liquid and gas phases in refractive index (1.35 vs. 1)

[19]. As shown in Figure 1, the output power and electrical level are small when the probe contacts the liquid phase, and large when the probe contacts the gas phase. The different results are attributable to the difference in refractive index between the two phases. Therefore, the output power and electrical level of the received light can be used to judge whether the phase contacted by the probe is liquid or gas.

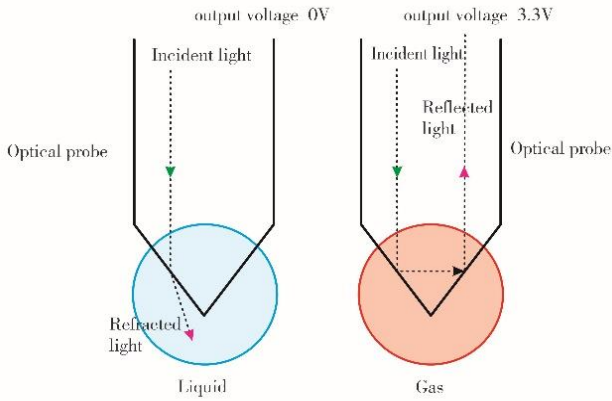


Figure 1. Working principle of optical sensor

### 2.2 Sensor design

As shown in Figure 2, each optical sensor consists of a light emission circuit, a high-sensitivity probe, and a light detection circuit. Specifically, the light emission circuit generates a visible light (wavelength: 400~600nm) on a high brightness light-emitting diode (LED), and then transmits the light to the high-sensitivity probe via the incident fiber; the high-sensitivity probe (diameter: 400 $\mu$ m; tip angle: 20~30 $^\circ$ ) is made of sapphire, a dampproof material, to mitigate the negative impact of humidity on detection accuracy; the light detection circuit receives the light reflected by the emergent fiber, converts the light signals into electric signals with a photodiode, and amplifies the voltage of electric signals (corresponding to the intensity of light signals) via an amplifier.

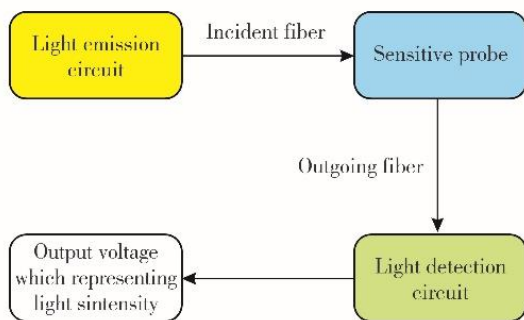


Figure 2. Structure of optical sensor

### 3. WORKING PRINCIPLE

Our bubble shape detector measures the volume and velocity of bubbles in CBM production wells according to the intensity of reflected light signals in the gas-liquid two-phase flow. The structure of the detector is illustrated in Figure 3.

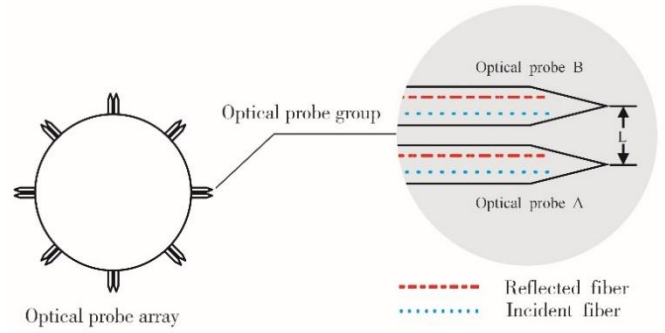


Figure 3. Structure of the bubble shape detector

Before use, the pup joint of the detector was connected to the tubing. To ensure the detection accuracy, eight sensor groups were arranged on the tubing at equal intervals along the circumference of the pup joint, forming an optical sensor array.

Each sensor group contains two optical sensors, denoted as A and B. The two sensors were installed in a stainless-steel sleeve. The end of incident fiber of one sensor was connected to the end of emergent fiber of the other sensor, and the probes of the two sensors were separated by a distance of L. Then, the sleeve was attached to the tubing.

### 3.1 Detection of bubble velocity

The bubble velocity was detected based on the data collected by both sensors A and B. Taking the probe tip of sensor B as the start point and the probe tip of sensor A as the end point, the moment the probe of sensor B contacted with bubble was defined as time  $t_0$ , the moment the probe of sensor A contacted with bubble as time  $t_1$ , the moment the probe of sensor B detected liquid as time  $t_2$ , and the moment the bubble went out of the detection range of sensor A as  $t_3$ .

Then, the four time points could be determined based on the electrical levels outputted by the circuits of the two sensors: the circuit of sensor B outputs a high electrical level at  $t_0$  and from  $t_0$  to  $t_1$ , and a low electrical level at  $t_2$ ; the circuit of sensor A outputs a high electrical level at  $t_1$ , and a low electrical level at  $t_3$ .

Figure 4 presents the theoretical waveforms outputted by sensors A and B during the detection of bubble velocity.

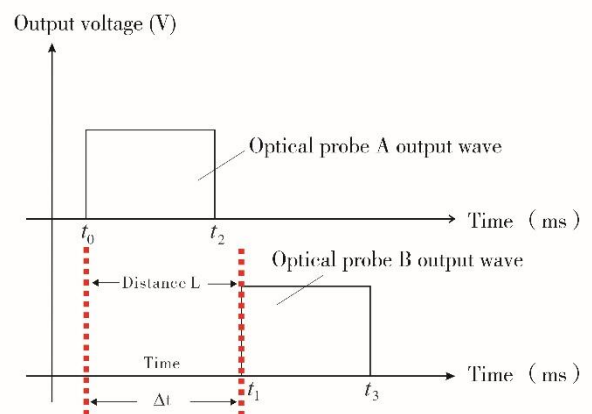


Figure 4. The theoretical waveforms outputted by sensors A and B during the detection of bubble velocity

The theoretical bubble velocity can be calculated by:

$$V=L/\Delta t \quad (1)$$

where,  $\Delta t=t_1-t_0$  is the time for the bubble to ascend by the distance of L.

### 3.2 Detection of bubble volume

The bubble volume was detected using the data collected by one of the two sensors. Taking the data of sensor, A for example, the moment the ascending bubble reached the probe of sensor A was defined as time  $t_1$ , and the moment the bubble went out of touch with the probe as time  $t_3$ . The circuit of sensor A outputs a high electrical level at  $t_1$  and a low electrical level at  $t_3$  (the light signals are weak due to the lack of contact).

Thus, the duration from  $t_1$  to  $t_3$  is the period, denoted as  $t_4$ , in which the bubble was detected by the sensor. The two time points were captured and the value of  $t_4$  was computed automatically by the STM32 microprocessor. On this basis, the bubble diameter could be derived by  $D=V*t_4$ . Assuming that the bubble is spherical, the bubble volume S can be expressed as:

$$S=4\pi r^3/3 \quad (2)$$

where,  $r=D/2$  is the radius of the bubble.

### 3.3 Determination of distance L

The distance L is of critical importance to the detection of bubble velocity and volume. If L is too small, the bubble will quickly pass from the probe of sensor A to that of sensor B.

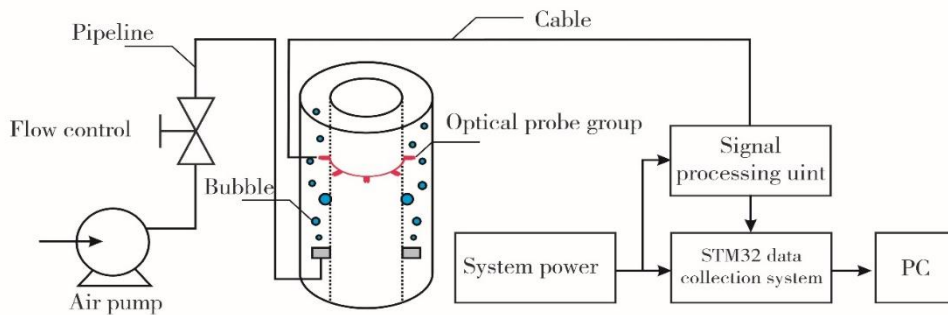


Figure 5. The simulation system

### 4.2 Simulation steps

The liquid in the wellbore annulus of CBM production well was simulated as 25°C clean water. The simulation was carried out in the following steps:

Step 1: Connect the air pump to the power supply and adjust the flow control valve, creating bubbles of different velocities and volumes.

Step 2: Connect the simulation system to the power supply, and initialize the STM32 microprocessor and the optical sensor detector.

Step 3: Take images of bubble motion with the standard bubble parameters acquisition device in the multiphase flow test system, and obtain the standard volume and velocity of each bubble using the image processing algorithm.

The short duration  $\Delta t$ , coupled with noises, will cause error to the data captured by the STM32, leading to inaccurate calculation of bubble velocity; If L is too large, many bubbles may pass between the two probes at the same time, inducing errors in the detected velocity.

Chabot et al. [20-21] carried out multiple experiments with the L values of 10.3, 9.5, 4.5, 2.0 and 1.0mm, respectively. The experimental results show that L=10.3, 9.5 and 4.5mm are too large, and that L=1.0 is too small. Inspired by their research and repeated experiments, the L value is selected as 2mm for our research.

## 4. SIMULATION

### 4.1 Simulation system

Figure 5 shows the simulation system of real-time bubble shape detection in the gas-liquid two-phase flow of CBM production wells. During the experiment, the bubbles were created by an air pump, and transmitted via a pipe into a flow control valve. The valve regulated the size and velocity of the bubbles. Then, the regulated bubbles moved along a pipe into a simulator of wellbore annulus of CBM production well, and started to ascend in the simulator. The ascending bubbles were detected by the optical sensor array, and the  $\Delta t$  value was obtained by the STM32 microprocessor. The captured data were filtered, denoised, and computed. The final results were transmitted to a personal computer, and displayed as bubble velocity and volume.

Step 4: Obtain the error between the bubble parameters measured by the proposed detector and the standard data acquired by the multiphase flow test system.

### 4.3 Results analysis

When the bubble has the same speed, if the bubble is small, the high-level time of the optical probe output signal is short; if the bubble is too large, the high-time time of the optical probe output signal is long.

#### 4.3.1 Analysis on the data of a single sensor

The data collected by a single sensor are plotted as the curves in Figure 6, where the two subgraphs respectively depict a single bubble and successive bubbles.

If the bubble velocity remains the same, the duration of high electrical level outputted by the sensor is positively correlated with the bubble volume.

In ideal conditions, the amplitude of the output signals is proportional to the intensity of the outputted light. To eliminate environmental interference, the output voltage was filtered, amplified and controlled within a set threshold, yielding a standard pulse waveform with an amplitude of 3.3V.

As shown in Figure 6, the amplitude of output signals was 0 when no bubble passed through the detection range, and was 3.3V when one or more bubbles passed through the detection range. Different modes of bubble motions displayed vastly different amplitudes, revealing that the optical sensor could effectively monitor the reflections of different media, and differentiate between gas phase and liquid phase.

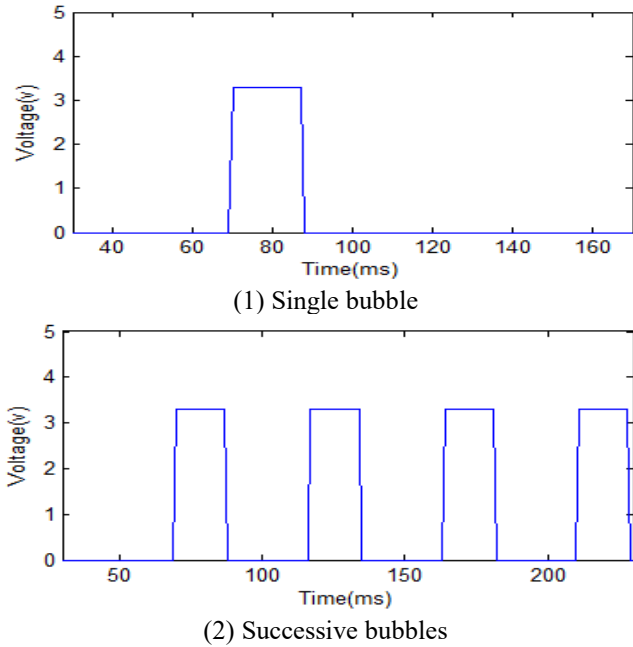


Figure 6. The simulation curve of a single sensor

4.3.2 Analysis on the data of two sensors

Under the bubble velocity of 0.261m/s and bubble volume of 113.81mm<sup>3</sup> (both were measured by our detector), the data collected by two sensors are plotted as the curves in Figure 7,

where the two subgraphs respectively depict the successive bubble curves of sensor B and sensor A.

It can be seen from Figure 7 that, for the same successive bubbles, sensor B detected the bubbles earlier than sensor A; for the same single bubble, the values of  $t_0$  and  $t_1$  could be obtained from the x-axis time differences of sensors A and B, and used to derive the volume and velocity of each bubble by formulas (1) and (2). The results show that the designed detector can measure bubble volume and velocity accurately.

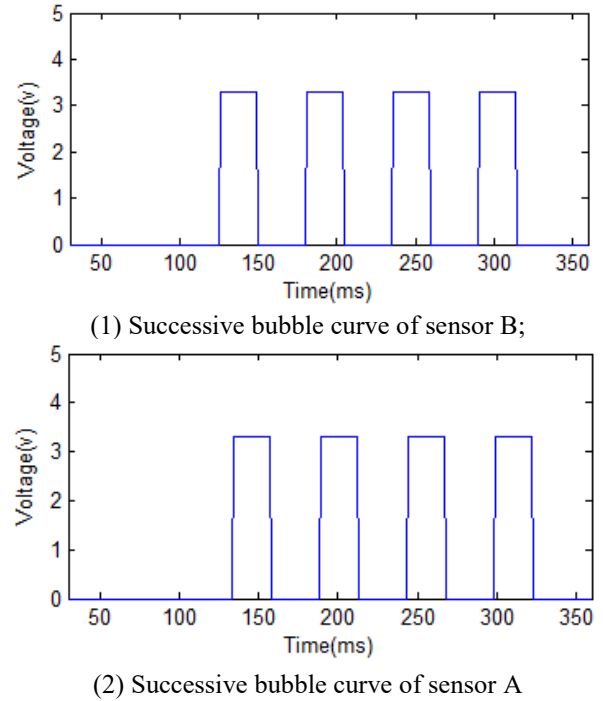
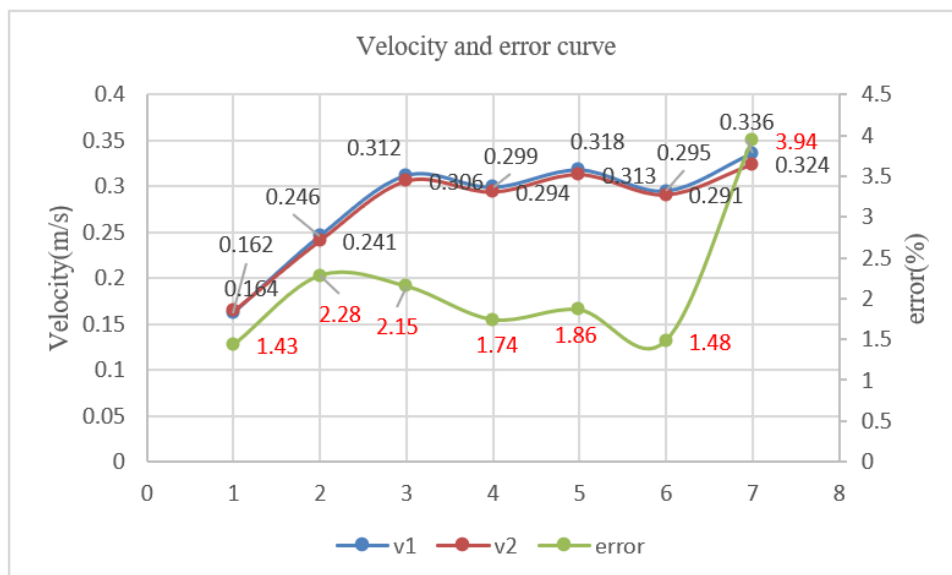
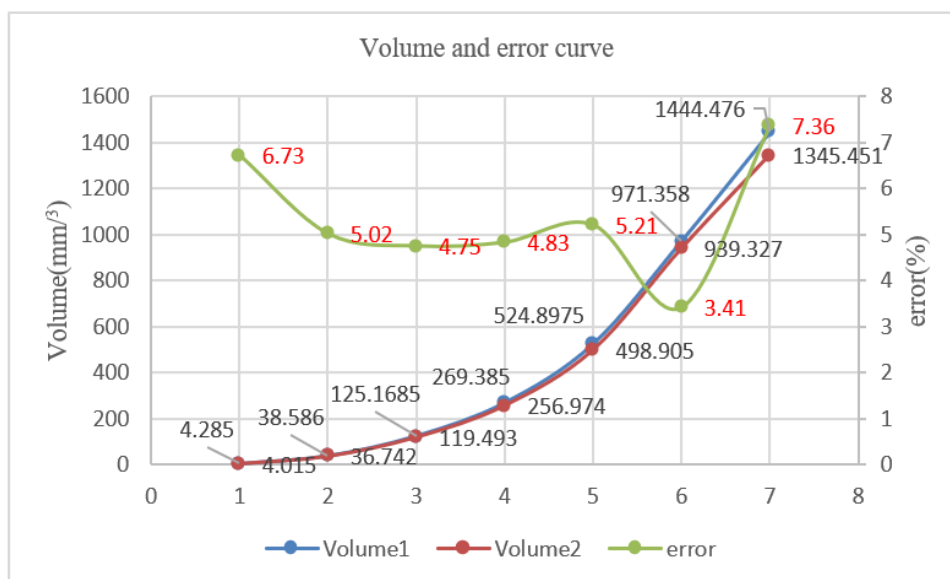


Figure 7. The simulation curves of two sensors

4.3.3 Comparative analysis

The bubble velocities and volumes obtained by our detector through the simulation were compared with those acquired by the standard bubble parameters acquisition device. Some of the comparative data are presented as Figure 8, where V1 and V2 are the bubble velocities captured by our detector and the standard device, respectively, and Volume 1 and Volume 2 are the bubble volumes acquired by our detector and the standard device, respectively.





**Figure 8.** Comparison of the bubble velocities and volumes obtained by our detector and the standard device

The comparison shows that, when applied to the CBM production well, our detector can measure the real-time bubble velocity with an accuracy of  $\pm 4\%$  and the real-time bubble volume with an accuracy of  $\pm 8\%$ . The volume error was slightly higher than the velocity error, because the volume is derived by formula (2) based on the velocity. Any error in velocity will induce an even larger error in volume. In addition, when a bubble becomes larger, it will pass through the detection range more rapidly. In this case, the velocity measurement will become less accurate, leading to a larger error in volume computation.

## 5. CONCLUSIONS

Our detector measures the real-time bubble velocity with an accuracy of  $\pm 4\%$  and the real-time bubble volume with an accuracy of  $\pm 8\%$ . While the traditional detectors can only identify the basic forms of bubble on the surface of media, our detector is able to work in  $<30\text{mm}$  annulus of CBM production wells.

Compared with the conductivity-based detector, our detector uses sapphire, a dampproof material, to mitigate the negative impact of humidity on detection accuracy. In addition, the probe does not react chemically with liquid, eliminating probe corrosion.

The future research will try to improve the measuring accuracy of bubble volume and velocity in the gas-liquid two-phase flow. A possible strategy is to process the data collected by the sensor array by the adaptive weighted mean filtering algorithm.

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## APPENDIX

$t_0$  — time of probe B starts to reach bubble, unit is ms

$t_1$  — time of probe A starts to reach bubble, unit is ms

$t_2$  — time of bubble leave probe B, unit is ms

$t_3$  — time of bubble leave probe A, unit is ms

$t_4$  — time of bubble passes through probe, unit is ms

$\Delta t$  — time of bubble travel distance between apex of probe A and B, unit is ms

$V$  — speed of bubble, unit is m/s

$L$  — distance between probe A and B, unit is mm

$S$  — bubble volume, unit is  $\text{mm}^3$

$D$  — bubble diameter, unit is mm

$R$  — bubble radius, unit is mm