



Comparison of Different Fin and Tube Compact Heat Exchanger with Longitudinal Vortex Generator in CFU-CFD Configurations

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ABSTRACT

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Over the last decades several studies have searched for improved Fin and Tube Heat Exchanger (FTHE) designs capable of providing the best thermo-hydraulic performance. The present study aims at quantifying and comparing the thermo-hydraulic performance of different FTHE configurations. Six different designs were analyzed. The first FTHE consisted of an in-line circular tube arrangement and the last one was a FTHE with staggered oval tube with two pairs of Delta Winglet Vortex Generators (DWVG) in common flow up–common flow down (CFU-CFD) configuration. The best performance was obtained using DWVG in CFU-CFD orientation. This configuration enabled a 90% increase of the thermal performance factor when compared with the first case, using only two pairs of vortex generator's per tube.

1. INTRODUCTION

Fin and tube compact heat exchanger (FTHE) is one of the most common types of compact heat exchanger. Commonly, FTHE uses fins on the air side to enhance compactness. The tubes can be individually finned or share one single continuous larger fin. FTHE can withstand high pressures on the tube side, and the operating temperature is limited by the type of bonding, materials employed and material thickness. Due to these characteristics, they are used in air-conditioning, refrigeration, airplanes, automobiles, heat pumps, among many other applications [1, 2].

Vortex Generators (VGs) can be employed as a way of increasing the heat transfer rate in FTHE. VGs are protrusions from a surface that intensify the heat transfer interrupting boundary layers, developing vortices, mixing flow and causing flow destabilization on the air side. There are two types of VGs: Transverse (TVG) and longitudinal vortex generators (LVG). TVG develop transverse vortices which are perpendicular to the flow direction, while LVG generate longitudinal vortices that last over long distances in the flow channel, resulting in a more efficient heat transfer enhancement [3, 4]. The angle of attack, aspect ratio and LVG design have a significant effect on heat transfer enhancement, [5]. The delta winglet type is one of the most studied LVG, because causes a lower pressure loss when compared to other vortex generators [3].

Kwak et al. [6, 7] studied the effect of delta winglet VGs in staggered and in-line circular tubes arrangement. In their research, they built-in vortex generators with a common flow up (CFU) arrangement. Compared to the common flow down (CFD) configuration from Fiebig et al. [8], their experimental results showed larger heat transfer enhancement and lower pressure loss.

Changing the shape of the tubes is another passive technique. Fiebig et al. [9] conducted an experimental study where the local heat transfer with flat and circular staggered tubes was

measured for Reynolds between 600 and 3000. They also investigated the influence of LVG and found that FTHE with flat tubes presented a better heat transfer performance than circular tubes.

Another tube shape consists of an oval type for FTHE. Han et al. [10] examined oval and different circular tubes through numerical research. In addition, they applied another passive technique consisting of two types of fins: louvered and wavy fin. They concluded that the oval geometry improved the flow characteristics in the wake region. This configuration reduces the flow resistance, achieving a uniform temperature distribution in the fin.

Chu et al. [11] carried out a study in FTHE using oval tubes and various number of tubes from 2 to 5 with LVG's in form of delta winglets. The angle of attack of the LVG's by 30° had the best performance. Additionally, Chu et al. [11] state a relation between the Nusselt number and the number of tubes. For a higher amount of tubes, the Nusselt number and the friction factor decreased. Therefore, the fewer the tubes per row, the better the performance.

Similarly, a number of studies have described a connection between the shape and geometric parameters of LVG and heat transfer enhancement. Gentry and Jacobi [12] suggested a direct dependency between vortex strength and Reynolds, wing aspect ratio and wing attack angle. Moreover, Díaz and Valencia [13] analyzed the impact of LVG shapes. In their research, they performed a numerical analysis to study heat transfer and pressure loss in a FTHE with oval tube and laminar flow. They compared the influence of different types of LVG: delta-type, rectangular, elliptical and spoon-type, the delta winglet type showed the highest increase in heat transfer.

A number of studies has suggested that the influence of LVG geometric parameters on the heat transfer and flow characteristics is correlated to the FTHE configuration. In an in-line circular tube and DWVG type configuration an angle of 45° showed the highest heat transfer enhancement for low Reynolds [14]. Lei et al. [15] obtained different results, they

compared different angles using Reynolds from 600 to 2600, but adding staggered circular tubes. Lei et al. [15] analyzed also the influence of the aspect ratio of the LVG, they combined these two parameters and concluded that for a two circular tube row with DWVG, the best performance was achieved with an aspect ratio of 2 and an angle of attack of 20°.

The amount of LVG in the flow channel also impacts the flow characteristics and heat transfer. Tiwari et al. [16] studied the impact of different configurations of DWVGs on heat transfer. In their research, they proposed various configurations of winglet pairs. The span-average Nusselt number was calculated and they concluded that the more LVG pairs, the better the heat transfer, along with a higher pressure loss. Recently, Carpio and Valencia [17] investigated a FTHE with a flat tube and multiple DWVGs, the configuration with 39 alternating LVG gave the highest thermal performance compared with the geometry without DWVGs with a 52% of increase on thermal-performance.

Chen et al. [18] combined CFD and CFU delta winglet VG orientation in an upstream configuration. They studied the effect of these arrangements in a fin and oval tube heat exchanger with an aspect ratio of 2, angle of attack of 30° and a fixed Reynolds of 300, LVG in staggered arrangement bring larger heat transfer enhancement than in in-line arrangement since the longitudinal vortices in the staggered arrangement influence a larger area and intensify the fluid motion normal to the flow direction. In the study of Salleh et al. [19] they have numerically investigated the thermal performance of LVG in CFD and CFU configuration in a model FTHE with four cylinders in line, LVG in CFU arrangement shows higher thermal and hydraulic performance for the three different LVG, however the base case without LVG was found to provide higher performance. This study shows that the increase in thermal performances using LVG is not always greater than one, and the optimal configuration for a FTHE depend on both cylinder and LVG arrangements and form. In the studies [4, 20] large numbers of compact heat exchanger studies have been compiled using VG until the year 2018. However, in the last year's new developed in this field are reported.

Shi et al. [21] have reported the optimal location of curved DWVG in a FTHE model with circular cylinder in a staggered arrangement for obtain high thermal performance, the curved DWVG showed higher performance as the straight DWVG, the maximum performance was 26% by a Reynolds number of 1000, and decrease dramatically with an increase on the Reynolds numbers to turbulent region. Modi and Rathod [22] compare sinusoidal wavy and elliptical curved RWVG in a model of FTHE with in line circular tube arrangement, in term of the values of area goodness factor (j/f), the base case without LVG have the best performance. Concave and convex curved LGV have been compared by Song et al. [23], the thermal performance was not always greater than one and the effect of the cylinder was not considered. The effect of attack angle of concave and convex DWVG in a FTHE was investigated in Ref. [24] using the synergy principle, the thermal-performance decreases by 18% using the DWVG. Finally, H. Kobayashi et al. [25] have used topological optimization to obtain an optimal FTHE design using different LGV design, they obtain an area goodness factor (j/f) of 16% higher with the proposal design.

The purpose of this research is to investigate the enhancement between six different designs, to find out a superior performance, using a minimum quantitate of VGs pairs.

2. MODEL DESCRIPTION

2.1 Governing equations

The air is assumed to be incompressible with constant properties. Governing equations in the computational domain can be expressed as follows:

Continuity equation

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0 \quad (1)$$

Momentum equations

$$\rho \left(\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} \right) = - \frac{\partial P}{\partial x} + \mu \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2} \right) \quad (2)$$

$$\rho \left(\frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} \right) = - \frac{\partial P}{\partial y} + \mu \left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} + \frac{\partial^2 v}{\partial z^2} \right) \quad (3)$$

$$\rho \left(\frac{\partial w}{\partial t} + u \frac{\partial w}{\partial x} + v \frac{\partial w}{\partial y} + w \frac{\partial w}{\partial z} \right) = - \frac{\partial P}{\partial z} + \mu \left(\frac{\partial^2 w}{\partial x^2} + \frac{\partial^2 w}{\partial y^2} + \frac{\partial^2 w}{\partial z^2} \right) \quad (4)$$

Energy equation

$$\rho C_p \left(\frac{\partial T}{\partial t} + u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} + w \frac{\partial T}{\partial z} \right) = k \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} \right) \quad (5)$$

where,

$u \left[\frac{m}{s} \right], v \left[\frac{m}{s} \right], w \left[\frac{m}{s} \right], \rho \left[\frac{kg}{m^3} \right], t[s], P [Pa], \mu \left[\frac{Ns}{m^2} \right], C_p \left[\frac{J}{kgK} \right], k \left[\frac{W}{mk} \right]$ represent the velocity in three directions, density, time, pressure, dynamic viscosity, specific heat and thermal conductivity, respectively.

2.2 Validation model

To validate the present work, Lei et al. [15] study was replicated. Their geometry was chosen because it represents a typical FTHE and they use DWVG with staggered circular tubes, as shown in Figure 1. The dimensions are shown in Table 1.

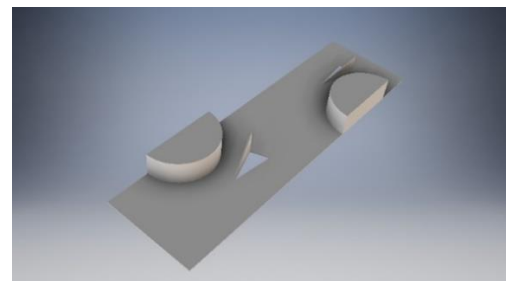


Figure 1. FTHE design proposed by Lei et al. [15]

Table 1. FTHE geometric details [15]

Dimension	Value
Transverse pitch (T_p) [mm]	12.7
Longitudinal pitch (L_p) [mm]	22
Fin pitch (F_p) [mm]	3.2
Fin thickness (F_t) [mm]	0.13
Tube outside diameter (D) [mm]	10.23
Air flow direction length (L) [mm]	44
DWVG angle of attack [$^\circ$]	20
Aspect ratio	2

2.3 FTHE designs

In this study, six FTHE different designs were proposed based on a heat exchanger with three rows of tubes. Every case is more complex than its precursor, starting with a plane fin without DWVG. The geometric parameters of the proposed FTHE are similar to the parameters of the validation FTHE. The new dimensions are circular tube outside diameter (D) of 10.207 [mm], air flow direction length (L) 70 [mm], and DWVG angle of attack of 30 [$^\circ$] in Figure 2.

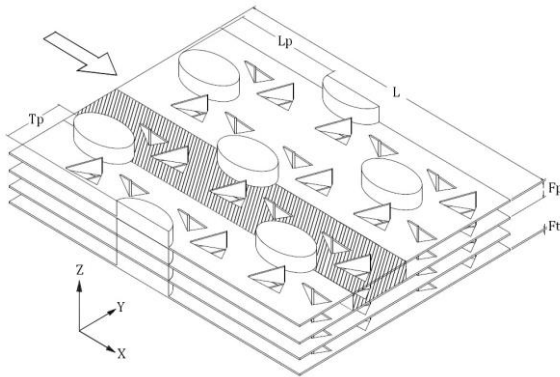


Figure 2. FTHE design

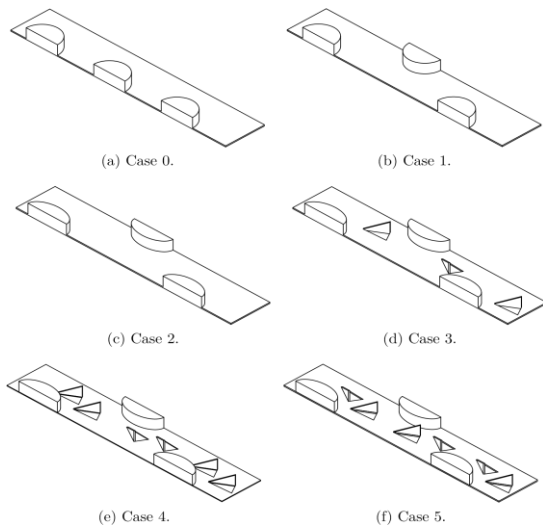


Figure 3 FTHE designs

Figure 3 shows the six different investigated cases. Figure 3 (a) shows Case 0 with in-line circular tubes and no LVG, (b) shows the Case 1 with staggered circular tubes and no LVG, and (c) shows a FTHE with staggered oval tubes and no LVG. The difference between Case 1 and Case 2 is the geometry of

the tubes, circular and oval tubes. In Figures 3 (d), (e) and (f) show a FTHE using staggered oval tubes with DWVG added in different quantities and orientations, in (d) only one pair of DWVG per tube in CFD orientation are used, in (e) two pairs of DWVG per tube in CFD-CFD orientation are added, and in (f) two pairs of DWVG per tube in CFU-CFD orientation are used.

The dimensions of the oval tubes were calculated based on the perimeter of the circular tubes, so the same heat transfer area was considered. In case 5, DWVG have the same parameters as DWVG in Case 4, changing only the orientation. Specific geometric dimensions are shown in Figures 4 and 5:

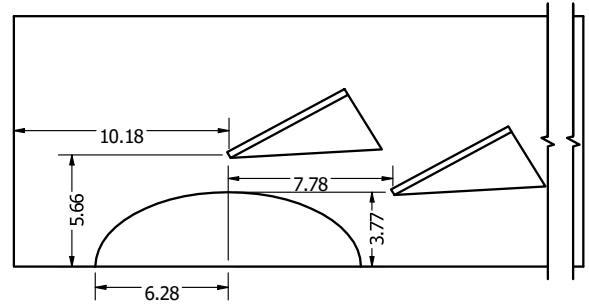


Figure 4. Case 4 geometric details in millimeters

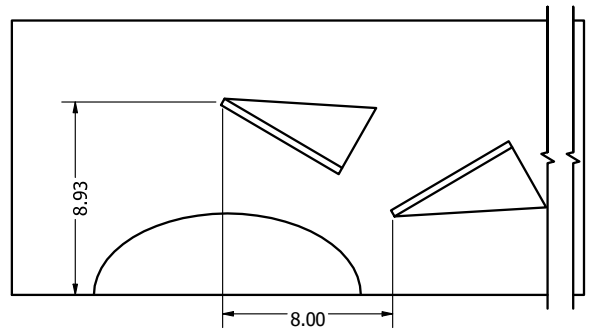


Figure 5. Case 5 geometric details in millimeters

2.4 Boundary conditions

The geometry was divided into three regions: upstream-extended, FTHE and downstream extended region. At the inlet boundary, u_{in} the velocity and T_{in} the air temperature are constant. For upper, lower and lateral boundaries in extended regions, a symmetry condition was set. Outflow and periodic condition were applied at outlet and LVG region respectively.

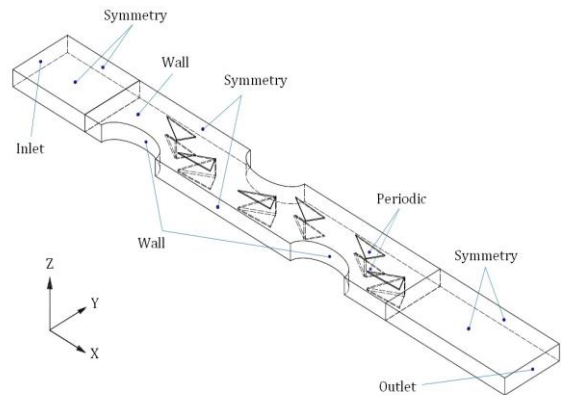


Figure 6. Boundary conditions on the computational domain

At the LVG basis a periodic boundary condition was applied, to simulate the interaction between the fins with LVG. To ensure there was not any flow recirculation, the exit domain was also extended five times the length of the heat transfer region. The computational domain and boundary conditions can be seen in Figure 6 where the extended regions were shortened. The air inlet temperature is $T_{in}=293$ K, the fin and tube have a wall temperature of $T_{wall}=313$ K, these temperatures are typically for FTHE. The inlet velocity was varied as 1.12 [m/s], 2.24 [m/s], 3.37 [m/s], 4.49 [m/s] and 5.61 [m/s] to obtain Reynolds number as 500, 1000, 1500, 2000 and 2500.

2.5 Parameters

The following relevant parameter definitions will be used in this investigation. The hydraulic diameter is defined in Eq. (6), considering A_o the total surface area, A_c is the minimum cross sectional area, and L is the air flow direction length [24].

$$D_H = \frac{4 \cdot LA_c}{A_o} \quad (6)$$

The Reynolds number is defined by the hydraulic diameter D_H and is shown in Eq. (7), and the velocity U_c is the velocity at the minimum cross section area.

$$Re = \frac{\rho \cdot U_c \cdot D_H}{\mu} \quad (7)$$

where, ρ , U_c and μ represent the density [$\frac{kg}{m^3}$], velocity [$\frac{m}{s}$] and dynamic viscosity [$\frac{kg}{m \cdot s}$], respectively.

The bulk temperature, as a function of the axial distance x , is shown in Eq. (8):

$$T_{bulk}(x) = \frac{\iint T(x, y, z) \cdot u(x, y, z) dy dz}{\iint u(x, y, z) dy dz} \quad (8)$$

The log-mean temperature difference LMTD was calculated using the Eq. (9):

$$LMTD = \frac{(T_{wall} - T_{in}) - (T_{wall} - T_{out})}{\ln \frac{(T_{wall} - T_{in})}{(T_{wall} - T_{out})}} \quad (9)$$

The average heat transfer coefficient can be determinate using Eq. (10):

$$h = \frac{\dot{Q}}{A_o LMTD} \quad (10)$$

\dot{Q} is the total heat transfer rate [W], to determine the local Nusselt number in the fin, the bulk temperature and the heat flux at each point on the fin are used, \dot{q} is reported by ANSYS Fluent 18.2 [26], as shown in Eq. (11).

$$Nu_{local}(x, z) = \left(\frac{\dot{q}(x, z)|_{y=0}}{T_{wall} - T_{bulk}(x)} + \frac{\dot{q}(x, z)|_{y=r_p}}{T_{wall} - T_{bulk}(x)} \right) \frac{D_H}{2k} \quad (11)$$

To determine the friction factor (f), the pressure difference and velocity U_c at the minimum cross section area are used, Eq. (12) shows the definition.

$$f = \frac{2 \Delta P}{\rho \cdot U_c^2} \cdot \frac{A_c}{A_o} \quad (12)$$

ΔP represent the pressure drop [Pa], to measure the efficiency of the increase in heat transfer when introducing LVG, the thermal performance JFw is used, as defined in Eq. (13), Carpio and Valencia [17]. The value of the base geometry is the Case 0, therefore, when the factor JFw is greater than 1, it indicates an increase in efficiency with respect to the Case 0.

$$JF_w = \frac{Nu/Nu_o}{(f/f_o)^{1/3}} \quad (13)$$

3. METHODOLOGY

3.1 Numerical method

Anslys Fluent 18.2 [26] was used to numerically simulate the different cases, the equations were iteratively solved using the finite volume method with SIMPLEC algorithm. The flow was considered laminar and we used transient simulations for a correct vortex development. The time step was set in $\Delta t = 10^{-5}$ [s], and the number of time steps was selected so the simulation reached a stationary state. The convergence criterion for every time step was residuals less than 10^{-6} and 10^{-3} for energy and momentum equations. Second order for the equation discretization were used.

3.2 Grid generation

The grid was generated using two types of elements: Tetrahedrons, for the actual heat transfer region consisting of a complex geometry, and hex dominant elements for extended parts, which do not require a finer grid. To improve the quality of the mesh system, "body sizing" was applied. Smaller elements were used on the heat transfer region, and the smallest elements were inside "spheres of influence", which were centered in the VGs for a better flow behavior analysis.

The resulting grid consisted of almost 430,000 elements. To ensure an optimal mesh quality the orthogonal quality and skewness criteria were considered. The topology of the mesh is displayed in Figure 7.

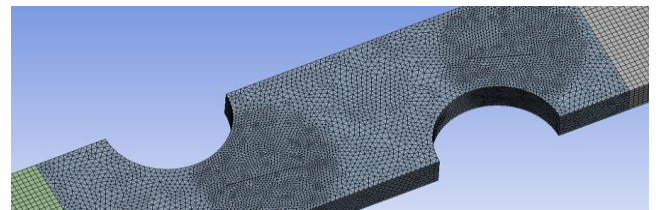


Figure 7. Details of the mesh

3.3 Grid independence

Three different meshes were analyzed, their characteristics are detailed in Table 2. The medium mesh is the one used in the validation model, and showed little variation compared

with that by Lei et al. [15]. The results obtained with the other meshes were compared with the medium grid and their values showed a difference of less than 5% on heat transfer coefficient and friction factor, thus proving the grid independence. The medium mesh provides precise results with lower computational times, and therefore was chosen.

Table 2. Details of the mesh

Category	Coarse Mesh	Medium Mesh	Fine Mesh
Elements	210,755	428,232	863,125
Nodes	39,883	78,826	156,567
SOI's elements size, mm	0.30	0.23	0.18
Max element size, mm	0.50	0.40	0.30

3.4 Validation results

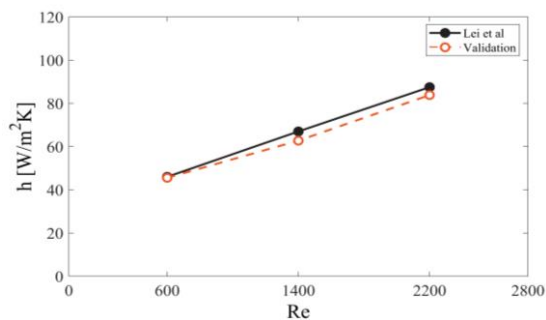


Figure 8. Heat transfer coefficient model validation

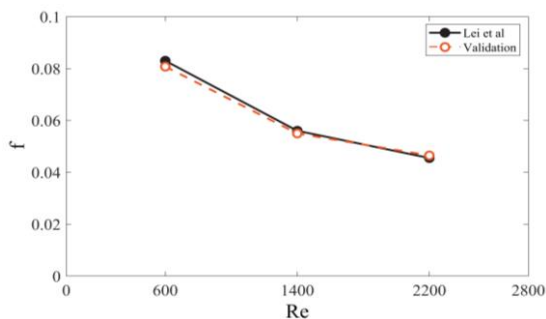


Figure 9. Friction factor model validation

The present work was validated with the numerical results obtained by Lei et al. [15]. To validate the results, the geometry described in Section 2.2 was simulated using the boundary conditions listed in Section 2.4. Fluid-solid conjugated heat transfer was modeled for the fin. The results of Lei et al. [15] was used as reference because they used a common geometry of FTHE without and with DWVG, and compare they numerical results with experimental data. Lei et al. [15] verify the numerical work with the model of FTHE without DWVG, they observed that the numerically predicted Colburn j-factor is about 1.5-7.8% higher than the experimental results, and the deviation of friction factor is between 1.6% and 9.2%.

The heat transfer coefficient and the friction factor values for Reynolds 600, 1400 and 2200 were compared. Both of them were calculated based on area averaged temperature using Eqns. (10) and (12) respectively. The Reynolds was expressed as Eq. (7).

The values obtained are shown in Figures 8 and 9. The results after the replication of Lei et al. [15] study showed a difference of less than 7% with the expected values, which is an acceptable difference.

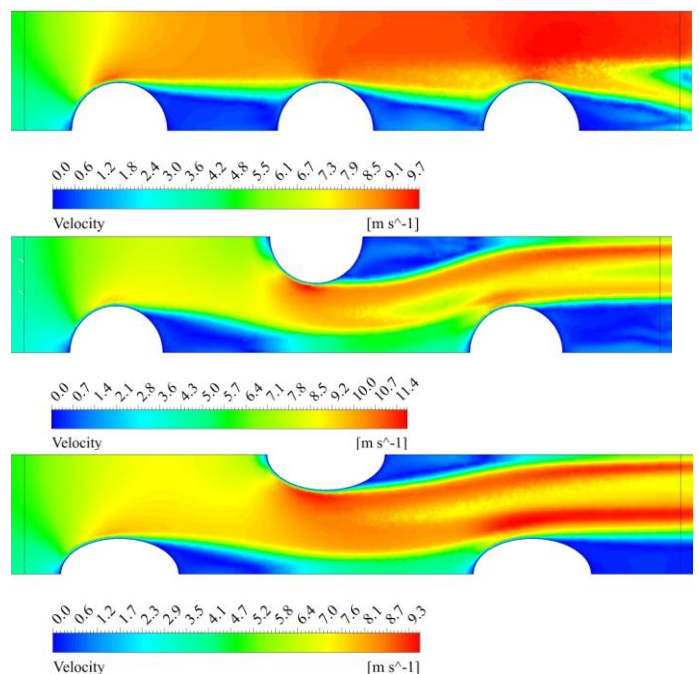
4. RESULTS

Figure 10 shows the velocity profile for the six investigated geometries without and with DWVG. A low velocity region can be recognized for Case 0, caused by the recirculation in the wake behind the tubes, this behavior inhibits the flow mix and does not contribute to the heat transfer. In the Case 1 the low velocity region after every tube is reduced because the tubes guide the flow into the wake region of the next row. In Case 2 staggered tubes are used but this time with oval shape, the change of shape has an impact on the wake region making it narrower so the low velocity region is even smaller than in Case 1.

In Case 3 DWVG generates longitudinal vortices that destabilize the flow and improve the mix even in dead water zones. In addition, because of their downstream position there is a smaller area for the air to flow between the DWVG and the tubes, which causes an increase in velocity as seen in Figure 10.

As a way of improving the heat transfer rate even more, two pairs of DWVG with CFD-CFD and CFU-CFD orientations were applied in Case 4 and Case 5, respectively. The higher the number of DWVG, the higher the flow mix. It is important to notice that, due to the generated longitudinal vortices the flow mix starts earlier on the channel, and their effect causes a thinner boundary layer after the third tube. In the Case 5 due the CFU-CFD DWVG orientation, the first DWVG (CFU) guides the flow to the next VG (CFD), resulting in a strong longitudinal vortex as seen in Figure 10.

The effects of DWVG on the temperature profile are showed in Figure 11 a), b) and c) for the Case 3, Case 4 and Case 5, respectively. DWVG produce a finer thermal boundary layer and mix the cold with the hot air and enhance the heat transfer after each DWVG. The Case 4 and 5 with two pairs of DWVG per cylinder showed the amplification of these effects on the thermal boundary layer.



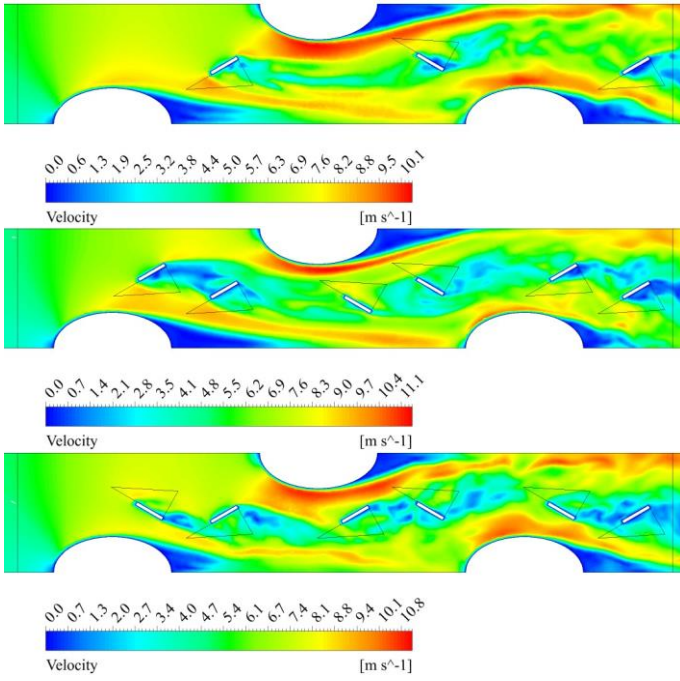


Figure 10. Velocity profile for Case 0, Case 1, Case 2, Case 3, Case 4 and Case 5, Reynolds number $Re=2000$

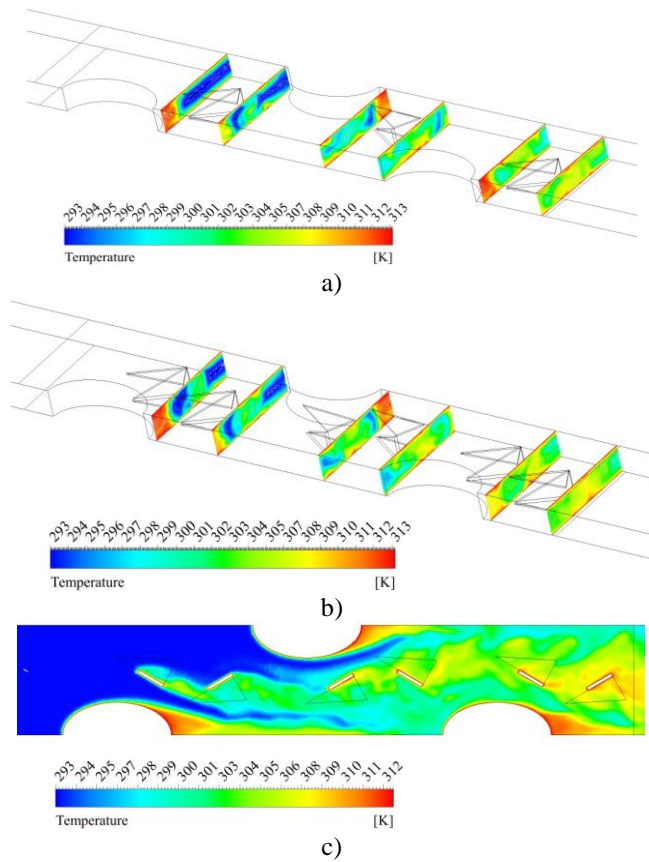


Figure 11. Temperature profile for a) Case 3, b) Case 4 and c) Case 5, Reynolds number $Re=2000$

The span average Nusselt number is plotted in Figure 12. The staggered arrangement (Case 1, 2, 3, 4 and 5) clearly shows a better performance because the second tube in staggered arrangement guides the flow to the wake of the preceding tube. The first peak shows a quite similar behavior depending on the shape of the tube. The second peak begins as

a consequence of the flow impact with the tube (for the cases without VGs). The curve in Case 2 reaches a lower second peak when compared to Case 1, but in Figure 13 the average Nusselt number is higher for Case 2. This implies that the heat transfer enhancement achieved thanks to the smaller stagnation zone of the first tube is greater than the increase in heat transfer caused by the horseshoe vortices generated by the second tube (which are stronger for the circular tube shape design). The presence of DWVG improves the span average Nusselt number due that the produced longitudinal vortices enhance the flow mix between tubes. Thus proving that the second and third peaks in cases 3, 4 and 5 are higher and also wider than in the previous cases 0, 1 and 2 without VGs.

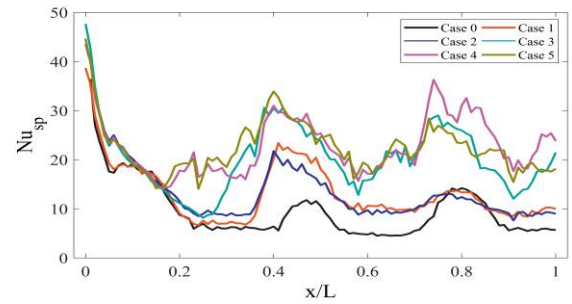


Figure 12. Span-average Nusselt number for Reynolds number $Re=2000$

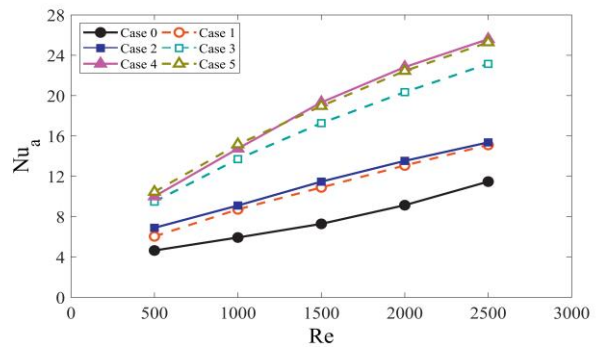


Figure 13. Average Nusselt number

The average Nusselt number is plotted in Figure 13 and it was calculated based on the span average Nusselt number (Eq. 11), and the exact values are shown in Table 3. As expected, the Nusselt value increases with the Reynolds due to higher velocities, stronger vortices and better flow mix. For higher Reynolds the addition of a second pair of DWVG produces a better heat transfer enhancement than for lower Reynolds, improving the Nusselt number by up to 30% compared with the one-pair DVWG design. The average Nusselt number for different Reynolds is very similar for Cases 4 and 5, heat transfer enhancement is affected in a similar way by the strength of the vortices generated by CFU-CFD DWVG (Case 5) and the number of vortices produced by CFD-CFD DWVG (Case 4). The Reynolds number was varied until the onset of turbulence, for Reynolds number $Re=2500$ we have simulated using the $k-\omega$ turbulence model, and the average Nusselt number and friction factor were the same as using the laminar model.

The friction factor is presented in Figure 14, and the exact values are shown in Table 3. The in-line tube without DWVG exhibits the lowest friction factor among all the cases. There is

only a slight difference between Case 1 and Case 2 in terms of f since both of them feature the same flow pattern. The augmentation of f in cases 3, 4 and 5 can be explained through the addition of DWVG; the longitudinal vortices generated produced an increase in the pressure loss. The higher the number of DWVG pairs, the greater the pressure loss. VGs orientation has an important effect on pressure loss, leading to an increment from 10% to 14% on the friction factor of the CFD-CFD configuration compared to CFU-CFD arrangement.

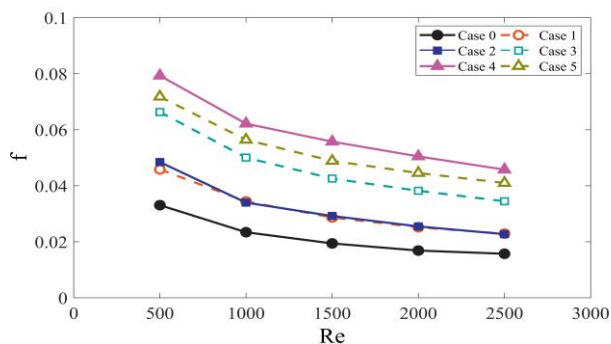


Figure 14. Friction factor

Table 3. Average Nusselt number and friction factor for Reynolds number

Case	Re	Nu	f
Case 0	500	4.65	0.0331
	1000	5.94	0.0234
	1500	7.29	0.0194
	2000	9.14	0.0169
	2500	11.48	0.0157
Case 1	500	6.05	0.0458
	1000	8.72	0.0344
	1500	10.90	0.0287
	2000	13.08	0.0252
	2500	15.11	0.0229
Case 2	500	6.90	0.0485
	1000	9.11	0.034
	1500	11.47	0.0292
	2000	13.53	0.0255
	2500	15.37	0.0227
Case 3	500	9.49	0.0663
	1000	13.71	0.05
	1500	17.27	0.0426
	2000	20.35	0.0382
	2500	23.15	0.0345
Case 4	500	10.01	0.0793
	1000	14.75	0.0622
	1500	19.33	0.0557
	2000	22.83	0.0505
	2500	25.60	0.0458
Case 5	500	10.46	0.0718
	1000	15.17	0.0564
	1500	18.97	0.0489
	2000	22.44	0.0445
	2500	25.28	0.041

The JFw thermal-dynamic efficiency factor compared every geometry with the base case (Case 0) considering the effects of heat transfer and the associated pressure loss is showed in Figure 15. The best performance for every Reynolds studied is achieved in Case 5. The results obtained for the JFw factor shows that all the geometries have a higher efficiency as the FTHE with circular cylinder in-line. Every geometry showed a better performance than the preceding design for every

Reynolds. The difference between the JFw factor in Case 4 and 5 is more substantial for lower Reynolds and the JFw factor converge into a value of 1.6 approximately for Reynolds 2500. Finally, the best performance is found in Case 5 for a Reynolds of 1500, where the JFw factor is 1.9 times larger than the first case.

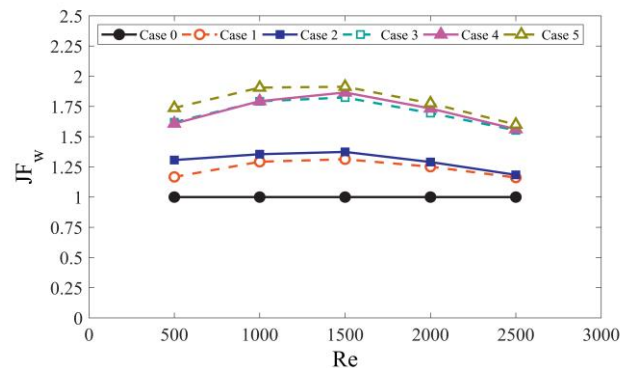


Figure 15. JFw for different cases

5. CONCLUSIONS

The purpose of this study was to investigate the thermo-hydraulic performance of six different FTHE configurations. The best performance was obtained in a FTHE with staggered oval tubes and two pairs of DWVGs in CFU-CFD orientation. When compared with the first case (in-line circular tubes), showed an enhancement of 90% in the thermal performance.

The staggered arrangement improved the mix flow in recirculation zones compared with in line arrangement, because every tube guided the flow to the wake of the preceding tube. Oval tubes showed a better performance than circular tubes. Finally, the addition of DWVG showed the highest impact on the flow and heat transfer. Indeed, the implementation of one pair of VGs per tube increased the JFw by 30% in Case 3 compared to Case 2 which did not have any VGs.

Even though Case 4 -staggered oval tubes with two pairs of DWVG in CFD-CFD orientation- exhibited the higher average Nusselt number, the generated vortices also increased the pressure loss, reaching a higher pressure loss than with the CFU-CFD orientation, where fewer but stronger vortices were identified. The best performance is a balance between heat transfer and pressure loss and was found in the configuration with CFU-CFD DWVG, obtained a 90% of increase in thermal performance using two VGs pairs per tube.

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NOMENCLATURE

A_c	minimum cross sectional area, m^2
A_0	total surface area, m^2

D_H	hydraulic diameter, m
c_p	specific heat, $J \cdot kg^{-1} \cdot K^{-1}$
f	friction factor
g	gravitational acceleration, $m \cdot s^{-2}$
h	heat transfer coefficient, W/m^2K
k	thermal conductivity, $W \cdot m^{-1} \cdot K^{-1}$
JFw	thermal performance
L	air flow direction length, m.
LMTD	log-mean temperature difference, K
Nu_{sp}	span-average Nusselt
p	pressure, Pa
\dot{q}	heat flux, W/m^2
\dot{Q}	total heat transfer rate, W
Re	Reynolds number

t	time, s
T	temperature, K
u	velocity, m/s
v	velocity, m/s
w	velocity, m/s
x	coordinate, m
y	coordinate, m
z	coordinate, m

Greek symbols

ρ	Density, kg/m^3
μ	dynamic viscosity, Ns/m^2