

Impact of Activation Energy in Darcy-Forchheimer Flow of Cross Nanofluid over a Radial Stretching Surface with Viscous Dissipation and Joule Heating



Cherlacola Srinivas Reddy¹, Besthapu Prabhakar^{2*}

¹ Department of Mathematics, ABV Government College, Janagaon 506167, Telangana, India

² Department of Mathematics, Kakatiya Government College, Hanamkonda 506001, Telangana, India

Corresponding Author Email: prabhakarbesthapu@gmail.com

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ABSTRACT

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This framework analyzes the impact of activation energy (AE) and binary chemical reaction (BCR) in Darcy-Forchheimer flow of cross fluid with nanoparticles due to radially stretched surface. Moreover slip, joule heating and viscous dissipation aspects have been considered. Ordinary differential equations acquired from the modelled governing partial differential equations with the assistance of suitable transformations. Further the system of nonlinear equations is computed numerically by Runge-Kutta-Fehlberg method cum shooting technique. Graphical representation has been given to analyze the velocity, temperature and concentration fields with the effect of various pertinent parameters. It is evident that inertia coefficient declines the velocity. Velocity decays for larger Weissenberg number while opposite trend observed in temperature field. Temperature field rises for augmented values of Eckert number. Concentration increases with increase of energy parameter.

1. INTRODUCTION

The study of non-Newtonian liquids flow and their features grab the attention of many researchers and scientists due to their significant applications in industrial products and procedures. Non-Newtonian liquids possess the non-linear relation between stress and strain. Depends on high viscosity few commonly used non-Newtonian fluids are toothpaste, lubricants, ketchup, silly putty, syrup, honey, paint, plastic, etc. Investigation of non-Newtonian flow field and its characteristics is quite difficult as compared to Newtonian liquids. To describe the features of non-Newtonian fluid flow by the well known Navier-Stokes equations are inadequate. Therefore, various fluid models have been suggested to demonstrate the features of non-Newtonian fluids. Cross [1] proposed Cross fluid model which is a major subclass of generalized Newtonian fluids and it predicts the shear thinning effects for both high and low shear rates. This fluid model has remarkable applications in engineering calculations due to the existence of the time constant. The empirical study of the cross fluid model was presented by Escudier et al. [2] by considering Cross equation with the non-Newtonian liquids carboxy methyl cellulose (CMC), xanthan gum (XG) and illustrated the fluid flow data. Xie and Jin [3] analyzed the free surface flow of the non-Newtonian fluid by WC-MPS method to find the four rheology parameters of Cross fluid model. Khan et al. [4] considered Cross fluid flow and heat transfer over a linear stretching surface and employed a numerical technique to solve boundary layer equations of the problem. From this study it is noticed that velocity profile is decreased with enlarging the Weissenberg number whereas inverse trend identified for the temperature field. Fluid flows through porous media have numerous applications corresponding to chemical engineering and geophysical systems. Such applications may

include movement of water in reservoirs fermentation process, crude oil production, grain storage, ground water systems, ground water pollution and recovery systems etc. The Darcy's law is reasonable under circumstances of low velocity and little porosity but it is inadequate whenever inertial and boundary features occur at higher velocity. Under such conditions it is impossible to neglect the inertia and boundary impacts. The non-Darcian porous medium is the revised form of Darcy law which includes the inertia and boundary effects. For higher velocity flow, the Forchheimer [5] formula is used in which squared velocity term has been added in the equation to predict the behavior of inertia and boundary effects. Muskat [6] termed this as "Forchheimer factor" which always reasonable for large Reynolds number. Darcy-Forchheimer flow of non-newtonian fluid was analyzed by Seddeek [7]. Pal and Mondal [8] studied influence of the Lorentz forces in a non-Darcy flow by considering variable viscosity. Shehzad et al. [9] considered Cattaneo-Christov heat flux model and homogeneous-heterogeneous reactions in Darcy-Forchheimer flow of Oldroyd-B fluid. Their analysis reveals that temperature is diminishing for Cattaneo-Christov heat flux model when compared to classical Fourier's law of heat conduction. Hayat et al. [10] examined Cattaneo-Christov model in flow of Maxwell fluid through a non-Darcy porous medium with temperature-dependent thermal conductivity. Fluids cooling and heating is the major issue in many industrial fields such as power manufacturing and transportation. Efficient cooling techniques are required to cool any kind of high energy equipment. The working fluids which are utilized in the industries have poor thermal conductivity due to this they cannot meet modern cooling challenges. Therefore, to improve the heat transfer capabilities of common heat transfer fluids Choi and Eastman [11] proposed the idea of nanofluids which is mixture of tiny

metallic particles in the base fluids. Nanofluids boost the thermal performance of the base fluids. Masuda et al. [12] noticed that thermal conductivity improvement by mixing the nanoparticles in the fluid. Buongiorno [13] established seven slip mechanisms in which he identified that Brownian diffusion and thermophoresis are two major influential factors which enhances thermal conductivity of the fluids. First time Khan and Pop [14] studied nanofluid flow over a stretched surface and obtained numerical solutions through Keller-box method. Makinde and Aziz [15] used convective boundary condition instead of constant heat flux and examined the boundary layer flow of nanofluid induced by a stretching sheet. A revised model is proposed by Kuznetsov and Nield [16] in which nanoparticles at the surface are passively controlled. Analysis of various thermo physical aspects of few non-Newtonian nanofluids given in the studies [17-20]. The consideration of mass transport with activation energy is attracted the investigators due to its vast usage in prominent areas like geothermal engineering, chemical engineering, oil emulsions and food processing. Activation energy is suggested by Arrhenius in 1889. It is the minimum required energy to be acquired by particles to experience a chemical reaction and this can be existing in the form of kinetic energy or potential energy and without the activation energy, reactants cannot produce products. Once the reaction starts activation energy of the system becomes zero. Generally, activation energy (AE) is denoted by E_a and written in Kj/mol or Kcal/mol. The applications of AE are very wide in geothermal engineering, chemical engineering, oil emulsions and food processing. Firstly Bestman [21] analyzed convective flow of binary amalgam in porous medium. AE and n^{th} order chemical reaction effects on time dependent radiated flat porous plate is investigated by Makinde et al. [22]. Alsaadi et al. [23] studied nonlinear mixed convective flow of non-Newtonian nanofluid over a porous stretching sheet under the impact of nonlinear radiation and activation energy and also, they discussed entropy generation rate. In this study they concluded that concentration increased with the effect of activation energy parameter. Unsteady flow of Carreau nanofluid is established by Irfan et al. [24] to acquire the effects of binary chemical reaction and activation energy. They reported the variations in both shear thinning and shear thickening fluids with the impact of reaction rate parameter and it shows the declined the concentration whereas it heightened for mounting values of activation energy parameter. Few recent investigations explore the characteristics of activation energy for various fluids [25-29]. In many practical applications the stretching sheet may not be linear, exponential because it can be stretched radially also in this context axisymmetric flow of fluids towards a radially stretched surface has got special interest due to its industrial applications like polymer extrusion, glass blowing etc. Ariel [30] examined second grade fluid due to radially stretching surface and further he obtained numerical and analytical solutions. Later slip flow of a fluid over a radially stretching sheet was studied by Ariel [31]. Investigations revealed that flow and heat transfer analysis of liquids [32-36] towards a radially stretching surface under various thermo-physical aspects. Khan et al. [37] reported Cross fluid past a radially stretching disk and they observed that velocity field exhibited the decreasing nature with the effect the local Weissenberg number. Most of the erstwhile studies reveal that flow geometries are confined to linear, nonlinear, exponential. Therefore, prime intention of this current study is to examine the aspects of activation

energy and chemical reaction on MHD flow of cross nanofluid over a radially stretching surface under simultaneous effects of viscous dissipation with joule heating, slip, convective condition and radiation. In addition to this zero normal flux condition is imposed at the sheet to spread the particles away from the sheet. Further detailed graphical analysis has been deliberated.

2. FORMULATION

Consider a steady Darcy Forchheimer flow of Cross nanofluid past a radially stretching surface placed at $z = 0$ and fluid resides in the region $z \geq 0$ with velocity $u = Uw = ar$, where a is positive number (see Figure 1). A uniform magnetic field B_0 imposed normal to the disk. The heat transport mechanism is presented in presence of convective heating with temperature T_f which gives a heat transfer coefficient h_f . Here T is the temperature of the fluid, T_∞ is the temperature far away from the disk. Furthermore, effects of viscous dissipation, joule heating and radiation are assumed in heat transfer. Impacts of AE and BCR are taken into consideration in mass transfer.

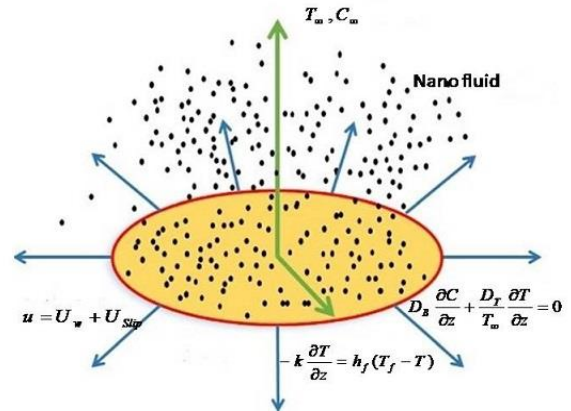


Figure 1. Geometry of the problem

By employing aforementioned aspects, the fundamental equations of mass, momentum, energy as well as concentration for Darcy Forchheimer flow of Cross nanofluid with AE and BCR are modeled as:

$$\frac{\partial u}{\partial r} + \frac{u}{r} + \frac{\partial w}{\partial z} = 0 \quad (1)$$

$$u \frac{\partial u}{\partial r} + w \frac{\partial u}{\partial z} = v \frac{\partial}{\partial z} \left(\frac{\frac{\partial u}{\partial z}}{1 + \left(\Gamma \frac{\partial u}{\partial z} \right)^n} \right) - \frac{\sigma B_0^2}{\rho} u - \frac{v}{K} u - \frac{C_b}{r\sqrt{K}} u^2 \quad (2)$$

$$u \frac{\partial T}{\partial r} + w \frac{\partial T}{\partial z} = \alpha \frac{\partial^2 T}{\partial z^2} + \tau \left[D_B \frac{\partial C}{\partial z} \frac{\partial T}{\partial z} + \frac{D_T}{T_\infty} \left(\frac{\partial T}{\partial z} \right)^2 \right] - \frac{1}{\rho c_p} \frac{\partial q_r}{\partial z} + \frac{\mu_0}{\rho C_p} \left(\frac{\left(\frac{\partial u}{\partial z} \right)^2}{1 + \left(\Gamma \frac{\partial u}{\partial z} \right)^n} \right) + \frac{\sigma B_0^2}{\rho} u^2 \quad (3)$$

$$u \frac{\partial C}{\partial r} + w \frac{\partial C}{\partial z} = D_B \frac{\partial^2 C}{\partial z^2} + \frac{D_T}{T_\infty} \frac{\partial^2 T}{\partial z^2} - K_r^2 \left(\frac{T}{T_\infty} \right)^n \exp \left(\frac{-E_a}{\kappa T} \right) (C - C_\infty) \quad (4)$$

With allied boundary conditions,

$$\left. \begin{aligned} u &= u_w(r) + u_{slip}, \\ w &= 0, -k \frac{\partial T}{\partial z} = h_f(T_f - T), \\ D_B \frac{\partial C}{\partial z} + \frac{D_T}{T_\infty} \frac{\partial T}{\partial z} &= 0 \text{ at } z = 0, \\ u &= 0, T = T_\infty, C = C_\infty \text{ as } z \rightarrow \infty \end{aligned} \right\} \quad (5)$$

Here velocity slip is $U_{slip} = l \frac{\frac{\partial u}{\partial z}}{1 + \left(\Gamma \frac{\partial u}{\partial z} \right)^n}$.

Here (u, w) signifies the velocity in radial- r and axial- z directions respectively, $F = \frac{C_b}{r\sqrt{K}}$, α is thermal diffusivity σ is electrical conductivity, ν is the kinematic viscosity, ρ is the density of the base fluid, D_B is the Brownian diffusion coefficient an D_T is the thermophoresis diffusion coefficient, $\tau = \frac{(\rho c)_p}{(\rho c)_f}$ is the ratio of nanoparticle heat capacity to the base fluid heat capacity. Using Rosseland approximation for radiation can write $q_r = -\frac{4\sigma^* \partial T^4}{3k^* \partial z}$ with σ^* is Stefan-Boltzmann parameter and k^* is denoted for mean absorption coefficient. Expansion of Taylor's series about the origin T_∞ and by ignoring the highest order expressions we get $q_r = -\frac{16\sigma^* T_\infty^3 \partial T}{3k^* \partial z}$ using this Eq. (3) takes the following form.

$$u \frac{\partial T}{\partial r} + w \frac{\partial T}{\partial z} = \alpha \frac{\partial^2 T}{\partial z^2} + \tau \left[D_B \frac{\partial C}{\partial z} \frac{\partial T}{\partial z} + \frac{D_T}{T_\infty} \left(\frac{\partial T}{\partial z} \right)^2 \right] + \frac{16\sigma^* T_\infty^3 \partial^2 T}{3k^* \rho c_p \partial z^2} + \frac{\mu_0}{\rho C_p} \left(\frac{\frac{\partial u}{\partial z}}{1 + \left(\Gamma \frac{\partial u}{\partial z} \right)^n} \right)^2 + \frac{\sigma B_0^2}{\rho} u^2 \quad (6)$$

Introducing the similarity variables,

$$\left. \begin{aligned} \eta &= \sqrt{\frac{\alpha}{\nu}} z, u = \alpha r f'(\eta), w = -2\sqrt{\alpha \nu} f(\eta), \\ \theta &= \frac{T - T_\infty}{T_f - T_\infty}, \phi = \frac{C - C_\infty}{C_\infty} \end{aligned} \right\} \quad (7)$$

By using Eq. (7), equation of continuity is trivially satisfied while Eqns. (2-4) and (6) are transformed into ODE form.

$$\begin{aligned} &[1 + (1 - n)(We f'')^n] f''' \\ &+ [2f f'' - (1 + Fr) f'^2 - (M \\ &+ Da) f'] \{1 + (We f'')^n\}^2 = 0 \end{aligned} \quad (8)$$

$$\begin{aligned} &(1 + Rd)\theta'' + Pr(2f\theta' + Nb\theta'\phi' + Nt\theta'^2) \\ &+ Pr \left[M Ec f'^2 \right. \\ &\left. + Ec \frac{f''}{1 + (We f'')^n} \right] = 0 \end{aligned} \quad (9)$$

$$\begin{aligned} &\phi'' + 2Sc f\phi' + \frac{Nt}{Nb} \theta'' \\ &- Sc \beta (1 + \delta_1 \theta)^n \exp \left(\frac{-E}{1 + \delta_1 \theta} \right) \phi \\ &= 0 \end{aligned} \quad (10)$$

Corresponding transformed boundary conditions are:

$$\begin{aligned} &f = 0, f' = 1 + \delta f''(0) \left\{ \frac{1}{1 + (We f''(0))^n} \right\}, \\ &\theta' = -\gamma [1 - \theta(0)], Nb\phi' + Nt\theta' = 0 \text{ at } \eta = 0, \\ &f' \rightarrow 0, \theta \rightarrow 0, \phi \rightarrow 0 \text{ as } \eta \rightarrow \infty \end{aligned} \quad (11)$$

The physical parameters appeared in above equations are Weissenberg number $We = \Gamma \alpha Re_r^{1/2}$, inertia coefficient $Fr = \frac{C_b}{\sqrt{K}}$ porosity parameter $Da = \frac{\nu}{Ka}$, magnetic parameter $M = \frac{\sigma B_0^2}{\rho \alpha}$, Radiation parameter $Rd = \frac{16\sigma^* T_\infty^3}{3k^* k_1}$, Prandtl number $Pr = \frac{\nu}{\alpha}$, Eckert number $Ec = \frac{u_w^2}{c_p(T_f - T_\infty)}$, Brownian motion parameter $Nb = \frac{\tau D_B C_\infty}{\nu}$, thermophoresis parameter $Nt = \frac{D_T(T_f - T_\infty)}{T_\infty \nu}$, energy parameter $E = \frac{E_a}{\kappa T_\infty}$, chemical reaction parameter $\beta = \frac{K_r^2}{a}$, temperature difference $\delta = \frac{(T_f - T_\infty)}{T_\infty}$, Schmidt number $Sc = \frac{\nu}{D_B}$, Biot number $\gamma = \sqrt{\frac{\nu h_f}{a k}}$.

Skin friction coefficient Cf_r and the local Nusselt number Nu_r are:

$$\begin{aligned} &Cf_r = \frac{(\tau_{rz})_{z=0}}{\frac{1}{2} \rho u_w^2}, \quad Nu_r = \frac{r q_w}{k(T_f - T_\infty)} \text{ where } (\tau_{rz})_{z=0} = \\ &\left[\eta_0 \frac{\frac{\partial u}{\partial z}}{1 + \left(\Gamma \frac{\partial u}{\partial z} \right)^n} \right]_{z=0}, q_w = -k \left(\frac{\partial T}{\partial z} \right)_{z=0}. \\ &\frac{1}{2} Re_r^{1/2} Cf_r = \frac{f''(0)}{1 + (We f''(0))^n}, Re_r^{-1/2} Nu_r = -\theta'(0) \text{ where} \\ &Re_r = \frac{u_w(r)r}{\nu}. \end{aligned}$$

3. METHODOLOGY

Nonlinear system (8-10) subject to (11) is computed numerically by Runge-Kutta-Fehlberg method cum shooting technique. To verify the present numerical outcomes, we have compared our numerical results of $-\theta'(0)$ with Butt and Ali [38] in Table 1.

Table 1. Comparison results of $-\theta'(0)$ for Newtonian case $We = 0$ and $Fr = 0$, $Da = 0$ and $Pr = 1$

M	γ	Ec	Butt and Ali [38]	Present results
0	0.5	0.5	0.21914	0.21913627
0.5			0.16621	0.16620886
1.0			0.11776	0.11776369
2.0			0.02992	0.02992232
1.0	0.1		0.03425	0.03424722
	0.2		0.06151	0.06151184
	0.5		0.11776	0.11776369
	1.0		0.16940	0.16940257

4. RESULTS AND DISCUSSION

This segment is presented to analyze the physical

implication of various fluid parameters M , Weissenberg number (We), porosity parameter (Da), inertia coefficient (Fr), Prandtl number (Pr), Eckert number (Ec), thermophoresis parameter (Nt), Brownian motion parameter (Nb), Schmidt number (Sc), chemical reaction parameter (β), energy (E), Biot number (γ), slip parameter (δ) on velocity $f'(\eta)$, temperature $\theta(\eta)$ and concentration fields $\phi(\eta)$. Table 1 is prepared to compare the present results with the existing literature. Figure 2 captured to examine the impact of M on $f'(\eta)$ and it elucidate that larger estimation of M decays the velocity field. Physically mounted values of M mean Lorentz force generates more resistance to the fluid therefore fluid velocity depreciates and reduces momentum boundary layer thickness. Effect of M on $\theta(\eta)$ is visualized through Figure 3. It is clear from the figure that $\theta(\eta)$ is enhanced with the stronger magnetic field. As the Lorentz force is resistive force which restricts the fluid motion. Therefore, more heat is produced and thus temperature raised in the working fluid. From the Figure 4 it is clear that $\phi(\eta)$ raises with the enlargement of M . Figure 5 demonstrates the characteristics of Weissenberg number We on velocity $f'(\eta)$. It is seen from the figure velocity deteriorates by uplifting the values of We for shear thinning fluid. Further it is noticeable from the Figure 6 and Figure 7 that cross nanoliquid temperature and concentration enhances for greater We . Physically, enlarging the values of the We causes enhancement in the relaxation time which results dwindle the velocity and rise in temperature. Figures 8-10 are plotted to examine the influence of δ on $f'(\eta)$, $\theta(\eta)$ and $\phi(\eta)$. Velocity profile exhibits decreasing trend for greater values of slip parameter while opposite tendency is noticed for $\theta(\eta)$ and $\phi(\eta)$. Figures 11-13 illustrates the influence of porosity parameter on $f'(\eta)$, $\theta(\eta)$ and $\phi(\eta)$. It has been observed that greater porosity parameter leads to lower velocity, higher temperature and concentration for the fluid.

Physically the existence of porous space enhances the resistance to liquid flow which results in increase in temperature and concentration. Figure 14 exhibits the behavior of velocity profile $f'(\eta)$ due to inertia coefficient Fr . It is evident that velocity declined for upsurging Fr and corresponding momentum layer gets thicker. Variation of velocity temperature and concentration field through power-law index n is examined in Figures 15-17. Figure 15 reveals that $f'(\eta)$ and momentum layer exhibits a progressive tendency for greater values of n but temperature and concentration field declined corresponding to uprising n (Figure 16 and Figure 17). In physical point of view shear-thinning liquid experiences low resistive force due to the low viscosity which causes for increment in the $f'(\eta)$ and declining of $\theta(\eta)$. Figure 18 reports the variation of $\theta(\eta)$ due to γ . An enlargement in γ causes stronger convection, consequently temperature increment is noticed.

Attribute of Ec displayed in Figure 19. Here greater Ec yields higher $\theta(\eta)$. Larger values of Ec causes to increase resistance in fluid motion as a consequence of this much heat is produced hence temperature profile increases. Influence of Nt on $\theta(\eta)$ and $\phi(\eta)$ is disclosed via Figure 20 and Figure 21. Clearly a rise in Nt augments temperature and concentration. Physically, thermophoresis force increases with enhancement of Nt due to these nanoparticles are being pushed towards cold zone from hot zone and hence increase in the Nt temperature and $\phi(\eta)$ increases. Figure 22 is sketched to discuss the variation of $\phi(\eta)$ due to Nb . It is detected that $\phi(\eta)$ exhibited decreasing tendency for greater values of Nb . It is happened due the uneven movement of nanoparticles in the

fluid. Figure 23 interprets the role of Rd on $\theta(\eta)$. From the figure it is described that larger values of radiation parameter enhance the temperature profile $\theta(\eta)$. Physically radiation process generates much heat in the liquid and corresponding thermal layer gets thicker.

Influence of E on $\phi(\eta)$ is discussed through Figure 24. It is noticed that concentration is increasing function of E . Physically, uplifting the values of E reduce the Arrhenius energy function which grows the generative chemical reaction, consequently $\phi(\eta)$ augmented. Figure 25 depicts the effects of chemical reaction rate β on $\phi(\eta)$. We observed that if we upgrade β a plummeting nature is observed in $\phi(\eta)$. Table 2 and Table 3 represents the variation in Skin friction coefficient Cf_r and the local Nusselt number Nu_r for various parameters.

Table 2. Numerical values of $Cf_r Re_r^{\frac{1}{2}}$ for various parameters

M	n	We	Fr	Da	δ	$Cf_r Re_r^{\frac{1}{2}}$
0.0	0.5	0.8	0.5	0.5	0.2	0.86428297
0.4						0.92602313
0.8						0.98085549
0.4	0.2					0.94573346
	0.4					0.93358237
	0.6					0.91720084
		0.1				1.20373753
		0.2				1.17220248
		0.3				1.13065507
			0.3			0.91052507
			0.6			0.93356439
			0.9			0.95541627
				0.1		0.86428297
				0.3		0.89613647
				0.5		0.92602313
					0.1	1.03252077
					0.2	0.92602313
					0.3	0.84031436

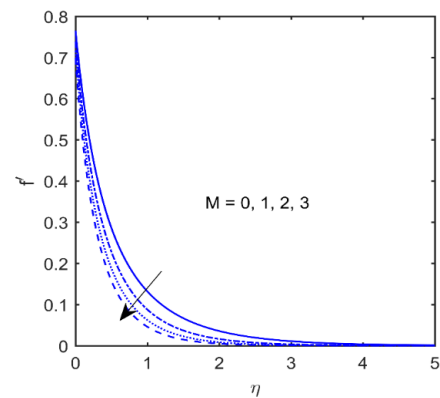


Figure 2. Variations of $f'(\eta)$ via M

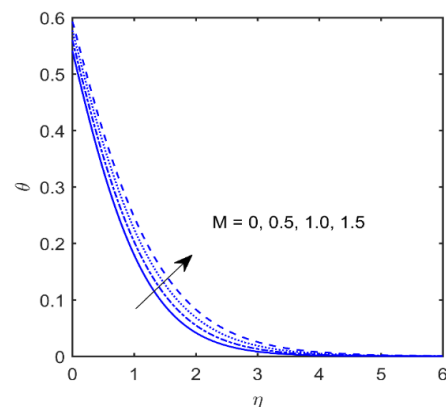


Figure 3. Variations of θ via M

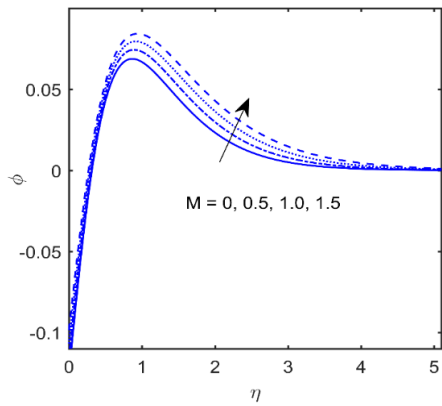


Figure 4. Variations of ϕ via M

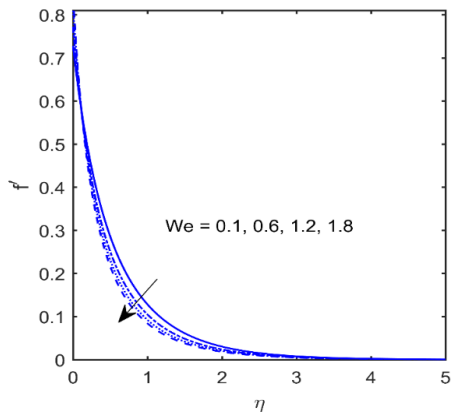


Figure 5. Variations of $f'(\eta)$ via We

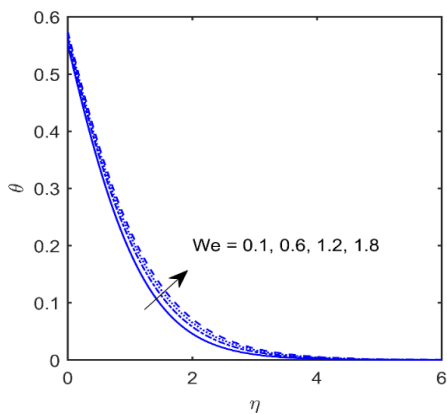


Figure 6. Variations of θ via We

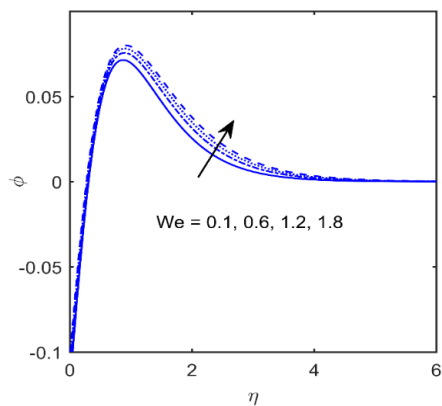


Figure 7. Variations of ϕ via We

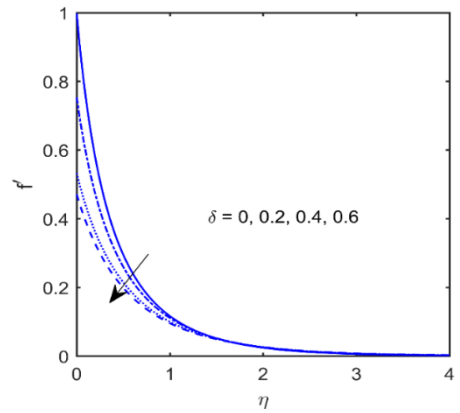


Figure 8. Variations of $f'(\eta)$ via δ

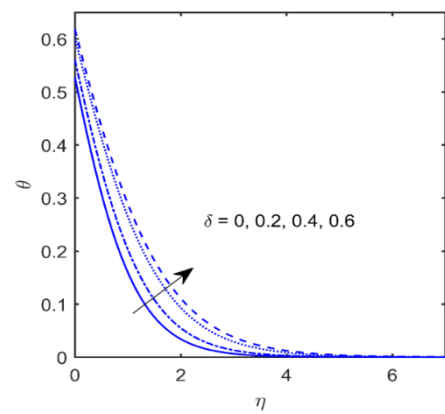


Figure 9. Variations of θ via δ

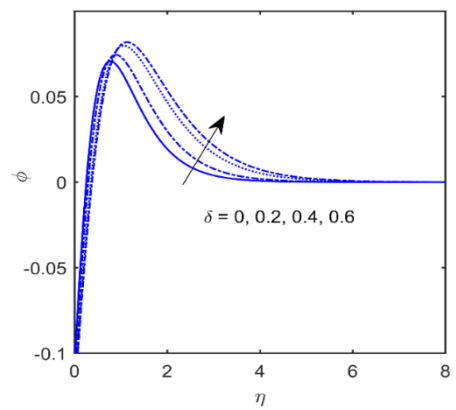


Figure 10. Variations of ϕ via δ

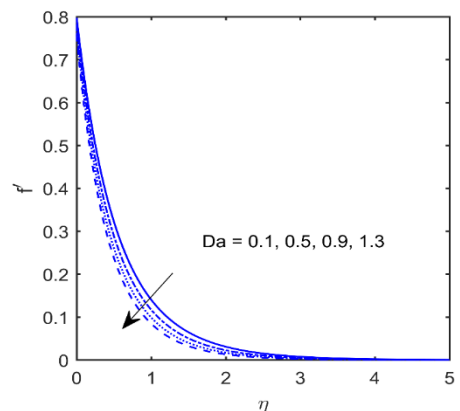


Figure 11. Variations of $f'(\eta)$ via Da

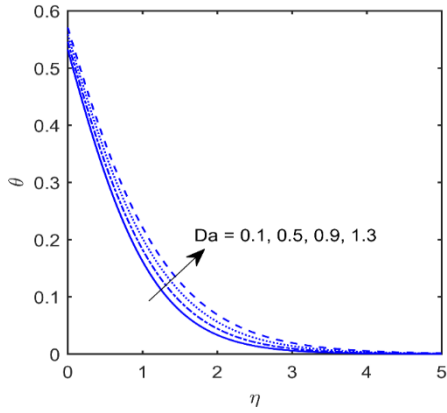


Figure 12. Variations of θ via Da

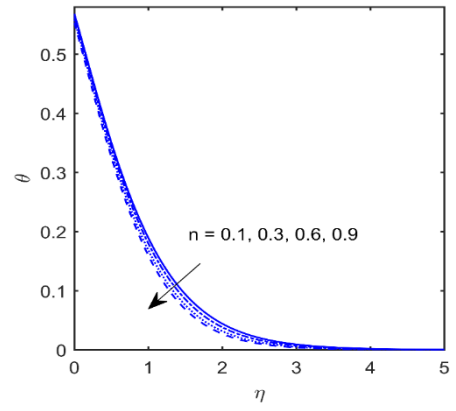


Figure 16. Variations of θ via n

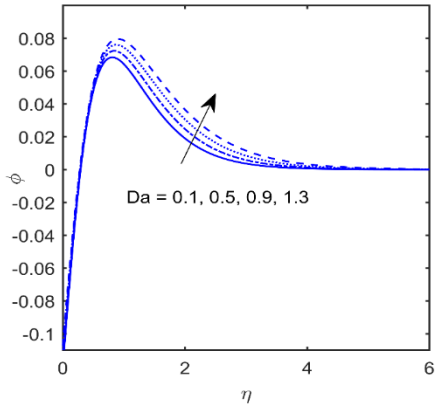


Figure 13. Variations of ϕ via Da

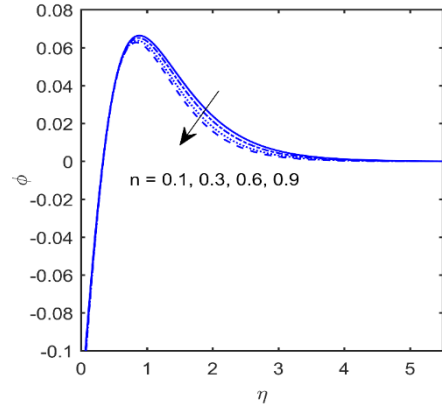


Figure 17. Variations of ϕ via n

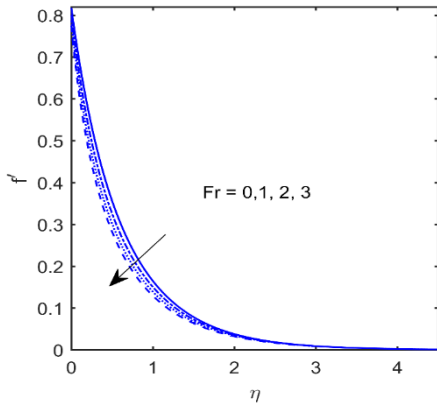


Figure 14. Variations of $f'(\eta)$ via Fr

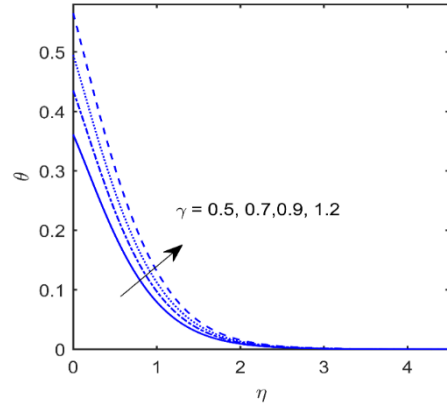


Figure 18. Variations of θ via γ

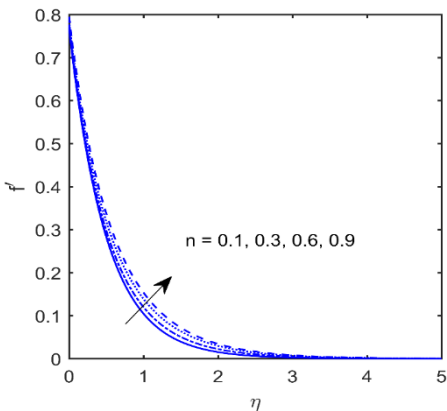


Figure 15. Variations of $f'(\eta)$ via n

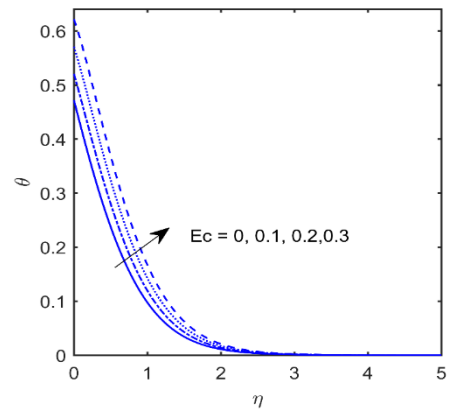


Figure 19. Variations of θ via Ec

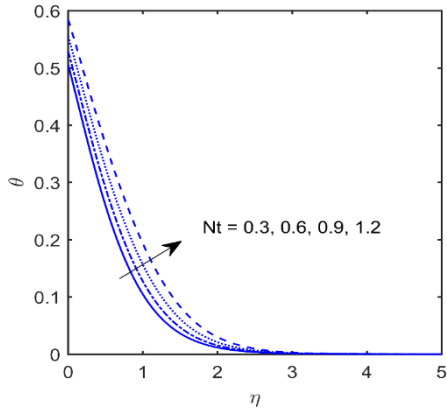


Figure 20. Variations of θ via Nt

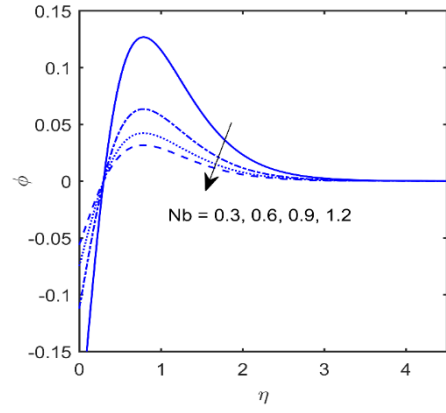


Figure 22. Variations of ϕ via Nb

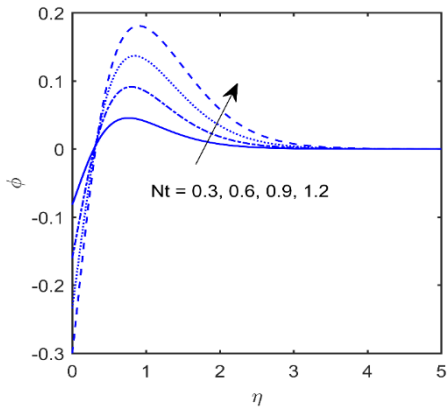


Figure 21. Variations of ϕ via Nt

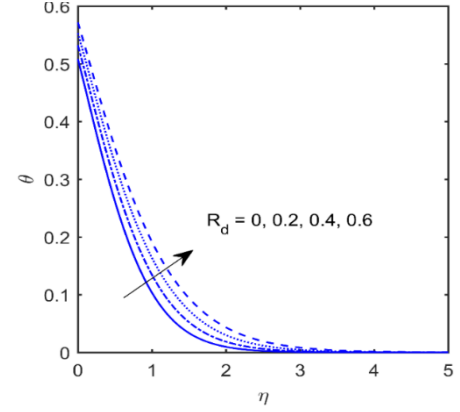


Figure 23. Variations of θ via Rd

Table 3. Numerical values of $Nu_r Re_r^{-\frac{1}{2}}$ for various parameters

M	n	We	Rd	Ec	Nt	Nb	E	B	γ	$Nu_r Re_r^{-\frac{1}{2}}$
0.0	0.5	0.8	0.25	0.1	0.3	0.3	1	1	0.6	0.40817062
	0.4									0.38939603
	0.8									0.37210942
	0.2									0.39024987
	0.4									0.38973814
	0.6									0.38897951
		0.1								0.40122524
		0.2								0.39821936
		0.3								0.39610769
			0.15							0.36689399
			0.25							0.38939603
			0.35							0.41094587
				0.0						0.42448060
				0.1						0.38939603
				0.2						0.35401764
					0.2					0.39368161
					0.4					0.38497444
					0.6					0.37570419
						0.2				0.38939603
						0.4				0.38939603
						0.6				0.38939603
							1			0.38939603
							2			0.38990527
							3			0.39003032
								1.5		0.38889180
								2.5		0.38799035
								3.5		0.38726308
									0.3	0.25066044
									0.4	0.30522449
									0.5	0.35081462

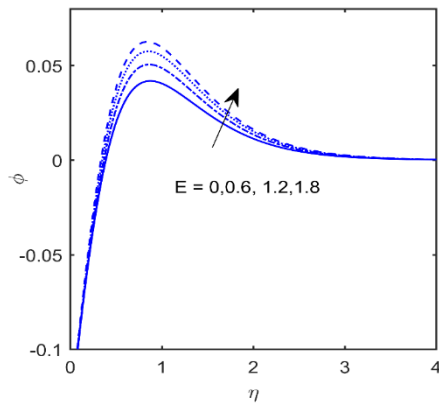


Figure 24. Variations of ϕ via E

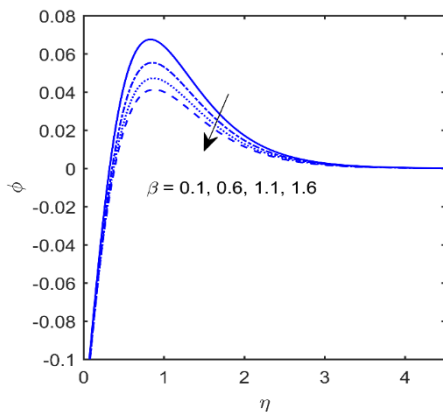


Figure 25. Variations of ϕ via β

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NOMENCLATURE

B_0	Strength of magnetic field
C	Nanoparticle volume fraction
C_f	Skin friction coefficient
C_p	Specific heat at constant temperature
Da	Porosity parameter
D_B	Brownian diffusion
D_T	Thermophoretic diffusion coefficient
E	Activation energy
Ec	Eckert number
f	Dimensionless stream function
Fr	Inertia coefficient
k	Thermal conductivity
M	Magnetic parameter
Nb	Brownian motion parameter
Nt	Thermophoretic parameter
n	Power law exponent
Pr	Prandtl number
Rd	Radiation parameter
Re_r	Reynolds number
Sc	Schmidt number
T	Temperature of fluid
u_w	Velocity of the stretching sheet
We	Weissenberg number
u, w	Velocity components in r and z directions

Γ	Time material constant	δ	Slip parameter
β	Chemical reaction parameter	δ_1	Temperature difference parameter
γ	Biot number	$(\rho c)_f$	Heat capacities of nanofluid
η	Similarity independent variable	$(\rho c)_p$	Effective heat capacity of the nanoparticle
ν	Kinematic viscosity		
ϕ	Dimensionless nanoparticle volume fraction	Subscripts	
ψ	Stream function	∞	Ambient condition
σ	Electrical conductivity	w	Conditions at the wall
ρ	Density		