

Deep Investigation on Natural Convection Flow of a Couple Stress Fluid with Nanoparticles in an MHD Vertical Porous Channel with Convective Boundary Conditions



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ABSTRACT

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This paper looks at the MHD natural convection flow through a vertical porous channel of couple stress fluid nanoparticles under convective heat conditions at the wall of the channel. Incorporated Soret and Dufour effects lead to strong coupled and highly nonlinear differential systems. To describe accurately all the physical phenomenon, the nanoparticle's volume fraction is taken into account. The useful technical of the similarity transformations is used to produce an ordinary system which is numerically solved. Graphical illustrations containing non-dimensional velocity, temperature, concentration and concentration of nanoparticles are extensively presented for different values of various thermophysical parameters. Main quantities of interest as Nusselt and Sherwood numbers at both the walls are tabulated.

1. INTRODUCTION

The flow of a non-Newtonian fluid with combined heat and mass transfer is frequently encountered in many engineering and industrial processes and it's increasingly used in several researches, recently, due to its wide range of applications like chemical engineering, environmental dynamics, cooling of electronic equipment, building ventilation and heat removal in nuclear technology.

Non-Newtonian fluids become very interesting for research because traditional Newtonian fluids cannot accurately describe the characteristics of actual promoted fluids, and their mechanics neglect the size effect of the material particles, which are included to improve the transfer rate of heat due to their higher thermal conductivity compared to the base fluid. The technical word 'nanofluid' was proposed for the first time by Choi and Eastman [1]. Nanofluids are used in many fields such as chillers, nuclear reactors, spacecraft, and heat exchangers to simulate the flow behavior of a lubricant with its own particles. Many theories of the micro-continuum have been generated, as the micropolar fluid model formulated by Eringen [2]. Heat transfer by nanofluid has been studied by many authors like Das et al. [3], and Das and Stephen [4], however Buongiorno [5] proposed an interesting mathematical nanofluid model based on the magnetic distribution effects in the absence of turbulent eddies, with Brownian diffusion and thermophoresis which are highlighted as the dominant slip mechanisms .

The couple stress fluid is a model of a non-Newtonian fluid whose theory is developed by Stokes [6, 7]. He proposed the micron-continuum theory with polar effects and defined the rotation field in terms of velocity field to establish the constitutive relationship between stress and strain rate. Synthetic fluids, polymers, animal blood, thickened oils, synovial fluid in synovial joints and suspension fluids are the fields of application of the couple-stress fluids [8-15].

The incompressible flows through a porous pipe of a couple

stress fluid have been studied recently and analyzed by several researchers [16-21]. The inertial effect should be significant at a higher rate and could be explained by the addition of a squared velocity term in the momentum equation, which is known as the Forchheimer extension of Darcy's law. A full detailed review of convective heat transfer, in Darcy and non-Darcy porous media, can be found in the book of Nield and Bejan [22]. Bujurke and Naduvinamani [23] studied the performance of a narrow porous bearing, lubricated with a couple stress fluid. Srinivasacharya and Kaladhar [24] based their studies on Hall and Ion-slip effects for the mixed convection flow of the couple stress fluid between two parallel plates. Akhtar and Shah [25] presented an analytical solution for unsteady flows of couple stress fluid between two parallel plates, while Ramesh [26] conducted a study on the effects of slip and convection conditions on the peristaltic flow of the couple stress fluid in a porous asymmetric channel. Kaladhar and Srinivasacharya [27] directed numerical and experimental studies of natural convection between vertical flat plates with asymmetric heating.

Recently, Hayet et al. [28] examined Soret and Dufour effects with chemical reaction of peristaltic motion of the MHD couple stress fluid with the convective conditions of heat and mass transfer in an inclined asymmetric channel.

When heat and mass transfer occur simultaneously in a moving fluid, the relationships between flows and drive potentials are closer. It has been observed that a flow of energy can be generated, not only by temperature gradients, but also by concentration gradients. The energy flow caused by the concentration gradient is called the thermo-diffusion effect (Dufour). In most studies of the heat and mass transfer process, the Dufour effect is neglected because of its order of magnitude which is smaller than the effects described by Fourier and Fick laws, but it can be considered as a secondary phenomenon. Srinivasacharya and Kaladhar [29] studied Soret and Dufour effects with the convective conditions of heat and mass transfer of the couple stress fluid through a semi-infinite

vertical plate. The same authors [30] studied the Soret and Dufour effects on steady free convective heat and mass transfer flow between two vertical parallel plates in couple stress fluid with chemical reaction. Eldabe et al. [31] examined the influence of Soret, Darcy, Hartmann and Schmidt numbers, and couple stress fluid parameter, on the heat and mass transfer with MHD flow of couple stress fluid through a porous medium. The irreversibility of heat and mass transfer of a couple stress nanofluid flow through a saturated magneto-porous vertical channel and a radiative heat transfer with entropy generation was realized in the papers [32, 33]. Mondal et al. [34], presented a study of heat and mass transfer for a stress-induced nanofluid in a magneto-porous medium with heat generation and thermal radiation. Rauf et al. [35] considered unsteady mixed convective flow in the presence of nanoparticles of stress fluid, over an oscillatory stretching sheet, with heat absorption/generation effects.

In all the studies above, no literature has been reported about nanoparticles concentration which is the aim of our work in this article. We will study heat and mass transfer effect of a couple stress nanofluid convective flow through two parallel walls packed with a saturated magneto-porous medium. A boundary value problem is obtained and suitable technique is used to solve the nonlinear problem. Soret and Dufour, Darcy and Forchheimer effects, the couple stress parameter S , Hartmann number M , thermophoresis parameter Nt , the Brownian motion parameter N_b are studied. The influence of the parameters that characterize the flow are given numerically through graphs and discussed afterwards.

2. MATHEMATICAL FORMULATION

Consider the hydromagnetic steady laminar free convection flow of an incompressible, electrically and thermally conducting couple stress with nanoparticle between two vertical permeable parallel plates spaced $2d$, in the presence of a uniform transverse magnetic field of strength B_0 applied parallel to y -axis.

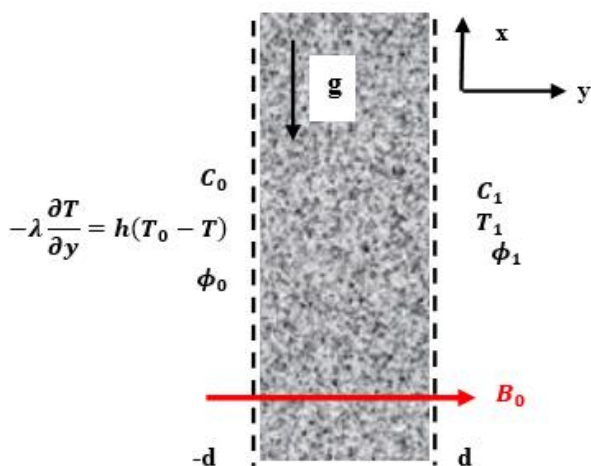


Figure 1. Physical configuration

The influences of external uniform magnetic fields of strength B_0 , transversally applied, are on the flow field. The effect of magnetic Reynolds number and the induced electric field are supposed to be minor and insignificant.

We assume that the left plate ($y = -d$) is convectively heated with hot fluid at temperature T_0 per heat transfer coefficient h ,

concentration C_0 and concentration of nanoparticles ϕ_0 , while the right plate ($y=d$) is exposed to a uniform temperature T_1 and a concentration C_1 and the concentration of nanoparticles ϕ_1 . The physical quantities depend only on the coordinate y because the boundaries in the x direction are of an infinite dimension, without loss of generality. The fluid properties are assumed constant whereas Dufour effect is taken into consideration. The physical model of the problem is presented in Figure 1.

With the above assumptions and Boussinesq approximations of energy and concentration, the equations governing the steady flow of an incompressible couple stress fluid are:

Continuity Equation:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \quad (1)$$

Momentum Equations:

$$\begin{aligned} -v_0 \frac{\partial u}{\partial y} = & -\frac{1}{\rho_f} \frac{\partial P}{\partial x} + \frac{\mu}{\rho_f} \frac{\partial^2 u}{\partial y^2} - \frac{\eta}{\rho_f} \frac{\partial^4 u}{\partial y^4} - \frac{\sigma B_0^2 u}{\rho_f} - \frac{\mu}{\rho_f K} u - \\ & - \frac{c_f}{\sqrt{K}} u^2 + (1 - \phi_1) g (\beta_T (T - T_1) + \beta_C (C - C_1)) - \\ & - g \left(\left(\frac{\rho_p - \rho_f}{\rho_f} \right) (\phi - \phi_1) \right) \end{aligned} \quad (2)$$

Energy Equation:

$$\begin{aligned} -v_0 \frac{\partial T}{\partial y} = & \frac{\lambda}{(\rho C_p)_f} \frac{\partial^2 T}{\partial y^2} + \frac{2\mu}{(\rho C_p)_f} \left(\frac{\partial u}{\partial y} \right)^2 + \frac{\eta}{(\rho C_p)_f} \left(\frac{\partial^2 u}{\partial y^2} \right)^2 \\ & + \varepsilon \frac{(\rho C_p)_p}{(\rho C_p)_f} \left[D_B \frac{\partial \phi}{\partial y} \frac{\partial T}{\partial y} + \frac{D_T}{T_m} \left(\frac{\partial T}{\partial y} \right)^2 \right] + \frac{D_m K_T}{C_s C_p} \frac{\partial^2 C}{\partial y^2} + \frac{\sigma B_0^2 u^2}{(\rho C_p)_f} \end{aligned} \quad (3)$$

Concentration Equation:

$$-\frac{1}{\varepsilon} v_0 \frac{\partial C}{\partial y} = D_m \frac{\partial^2 C}{\partial y^2} + \frac{D_m K_T}{T_m} \frac{\partial^2 T}{\partial y^2} \quad (4)$$

Concentration of nanoparticles Equation:

$$-\frac{1}{\varepsilon} v_0 \frac{\partial \phi}{\partial y} = D_B \frac{\partial^2 \phi}{\partial y^2} + \frac{D_T}{T_m} \frac{\partial^2 T}{\partial y^2} \quad (5)$$

The boundary conditions are:

$$u = 0 \text{ at } y = \pm d \quad (6)$$

$$u_{,yy} = 0 \text{ at } y = \pm d \quad (7)$$

$$-\lambda \frac{\partial T}{\partial y} = h_f (T_0 - T), C = C_0, \phi = \phi_0 \text{ at } y = -d \quad (8)$$

$$T = T_1, C = C_1, \phi = \phi_1 \text{ at } y = d \quad (9)$$

The boundary condition (6) corresponds to the classical no-slip condition from viscous fluid dynamics. The boundary condition (7) implies that the couple stresses are zero at the plate surfaces. The boundary condition (8) and (9) corresponds to the temperature, concentration and concentration of nanoparticles on the surfaces of the plate (-d) and (+d)

respectively.

where, u is the velocity component along x direction, T , C and ϕ represent the temperature, concentration and nanoparticles concentration respectively, v_0 is the fluid velocity, P defines the pressure, μ signifies the coefficient of viscosity, ρ_f and ρ_p mean the density base liquid and density of nanoparticle respectively, η denotes the couple stress viscosity parameter, β_T and β_C are the thermal expansion coefficient and the concentration expansion coefficient respectively, g is the acceleration due to gravity, σ is the electrical conductivity, B_0 denotes the magnetic field, K designates permeability of porous medium (hydraulic conductivity), c_f is the Forchheimer constant, λ is the thermal conductivity of the fluid, $(\rho C_p)_f$ and $(\rho C_p)_p$ are the heat capacity at constant pressure of fluid and the heat capacity of nanoparticles respectively, $\alpha = \lambda/(\rho C_p)_f$ represents the thermal diffusivity, ε is the porosity, D_B indicates the Brownian diffusion coefficient, in $D_T = D_m K_T$, D_T is the thermophoresis diffusion coefficient, D_m is the molecular solutal diffusivity, K_T indicates the thermal diffusion ratio, T_m is the mean temperature, C_s is the concentration susceptibility. h_f is the heat transfer coefficient between the plate and the hot fluid.

Introducing the following similarity transformations:

$$\begin{cases} \eta = \frac{y}{a}, X = \frac{x}{a}, u = \frac{v_f}{a} f, \theta = \frac{T - T_1}{T_0 - T_1}, \\ \varphi = \frac{C - C_1}{C_0 - C_1}, \psi = \frac{\phi - \phi_1}{\phi_0 - \phi_1} \end{cases} \quad (10)$$

After using these transformations, we obtain the following nonlinear system of the differential equations:

$$A + Re f' + f'' - S^2 f^{(4)} + Gr_T \theta + Gr_M \varphi - Nr Gr_T \psi - Mf - Da \cdot f - Fo \cdot f^2 = 0 \quad (11)$$

$$\theta'' + Re Pr \theta' + 2 Ec Pr f'^2 + Ec Pr S^2 f''^2 + Nb \theta' \psi' + Nt \theta'^2 + D_f Pr \varphi'' + Ec Pr M f^2 = 0 \quad (12)$$

$$\varphi'' + Re Pr Le_n \varphi' + S_r Sc / Pr \theta'' = 0 \quad (13)$$

$$\psi'' + Re Pr_n \psi' + Nt / Nb \theta'' = 0 \quad (14)$$

where, primes denote the differentiation with respect to η alone:

$$A = -\frac{\partial \bar{P}}{\partial X}; \text{ (the pressure gradient); where } \bar{P} = \left(\frac{a^2}{\rho_f v_f^2}\right) P.$$

$$Re = \frac{v_0 a}{\nu_f}; \text{ (the Reynolds number).}$$

$$S^2 = \frac{\eta}{\rho_f a^2 \nu_f}; \text{ (the couple stress parameter).}$$

$$Gr_T = \frac{(1-\phi_1)g \beta_T (T_0 - T_1) a^3}{\nu_f^2}; \text{ (The thermal Grashof number)}$$

$$Gr_M = \frac{(1-\phi_1)g \beta_C (C_0 - C_1) a^3}{\nu_f^2}; \text{ (The concentration Grashof number).}$$

$$Nr = \frac{(\rho_p - \rho_f)(\phi_0 - \phi_1)}{\rho_f (1 - \phi_1) \beta_T (T_0 - T_1)}; \text{ (The nanofluid buoyancy ratio parameter).}$$

$$M = \frac{\sigma B_0^2 a^2}{\rho_f \nu_f}; \text{ (The magnetic field parameter)}$$

$$Da = \frac{a^2}{K}; \text{ (Darcy number).}$$

$$Fo = \frac{c_f a}{\sqrt{K}}; \text{ (Forchheimer number).}$$

$$Pr = \frac{(\rho C_p)_f \nu_f}{\lambda}; \text{ (The Prandtl number).}$$

$$Ec = \frac{\nu_f^2}{(\rho C_p)_f a^2 (T_0 - T_1)}; \text{ (The Eckert number).}$$

$$Nb = \frac{(\rho C_p)_p \varepsilon D_B (\phi_0 - \phi_1)}{(\rho C_p)_f \alpha_f}; \text{ (The Brownian motion parameter)}$$

$$Nt = \frac{(\rho C_p)_p \varepsilon D_T (T_0 - T_1)}{(\rho C_p)_f T_m \alpha_f}; \text{ (The thermophoresis parameter).}$$

$$\text{With } \alpha_f = \frac{\lambda}{(\rho C_p)_f}; \text{ (The thermal diffusivity).}$$

$$D_f = \frac{D_m K_T (C_0 - C_1)}{\nu_f C_s C_p (T_0 - T_1)}; \text{ (the Dufour number).}$$

$$S_r = \frac{D_m K_T (T_0 - T_1)}{(C_0 - C_1) T_m \alpha_f}; \text{ (the Soret Number).}$$

$$Le_n = \frac{\alpha_f}{\varepsilon D_m}; \text{ (Thermo-nanofluid Lewis number).}$$

$$Pr_n = \frac{\nu_f}{\varepsilon D_B}; \text{ (The Prandtl nanofluid number).}$$

$$H = \frac{h_f a}{\lambda}; \text{ (The Biot number).}$$

The boundaries conditions (6)-(9) in terms of velocity $f(\eta)$, temperature $\theta(\eta)$, concentration $\varphi(\eta)$ and concentration of nano-particles $\psi(\eta)$ become:

$$\begin{aligned} f = 0; f'' = 0; \theta' = -H\theta; \varphi = 1, \psi = 1 \text{ at } \eta = 0 \\ f = 0; f'' = 0; \theta = 1; \varphi = 0, \psi = 1 \text{ at } \eta = 1 \end{aligned} \quad (15)$$

The physical quantities of interest are the local Nusselt and the local Sherwood numbers, which are defined as:

$$Nu = \frac{a q_h}{h(T_0 - T_1)}, Sh = \frac{a q_m}{D_m(C_0 - C_1)} \quad (16)$$

where, q_h denotes heat flux and q_m is the mass flux near the surface.

$$q_h = -h \left(\frac{\partial T}{\partial y}\right)_{y=0}, q_m = -D_m \left(\frac{\partial C}{\partial y}\right)_{y=0} \quad (17)$$

We obtain dimensionless version of these key design quantities:

$$Nu_{1,2} = -\theta'(\eta)|_{\eta=0,1}, Sh_{1,2} = -\varphi'(\eta)|_{\eta=0,1} \quad (18)$$

3. RESULTS AND DISCUSSION

The numerical and computational results are discussed through the graphical illustrations. The variation of Velocity, Temperature, Concentration and Concentration of nanoparticles for different values S_r and D_f numbers, Da and F_0 numbers, as well as S , M , Nt , Nb , Gr_T , Gr_M , Le_n , Nr and H , are studied and discussed through Figures [3-30]. The values used in the calculus are mentioned in each figure. Soret and Dufour numbers values are taken such as their product stay constant, meaning that the temperature T_m is kept stable [34]. Mathematical software is used to find out the numerical results.

In absence of the nanoparticles $Nt = Nb = Pr_n = Nr = 0$, and the model becomes classical couple stress fluid. For comparison, we put $Da = Fo = 0$ as without porous medium, the magnetic field $M=0$, the convective boundary conditions $H = 0$ and the pressure gradient is taking $A=0$. It's noted that $Br = Ec \cdot Pr$, then the flow-field profiles, generated

by the computer, of this study, are nearly similar with those of the results presented by Srinivasacharya and Kaladhar [29].

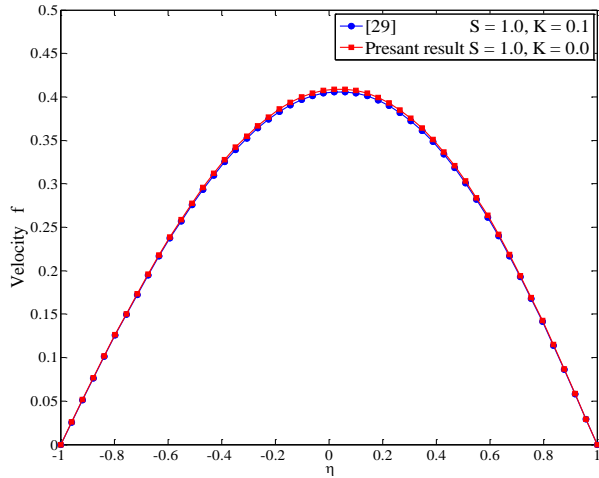


Figure 2. Comparison of velocity profile for the present result with Srinivasacharya's and Kaladhar [29] results

We have compared the present model to that of Srinivasacharya and Kaladhar [29] for two values of the couple stress parameter and for non-dimensional velocity. They are illustrated in Figure 2. The outcomes are found to be in good agreement. It can be observed from this figure that the two curves are almost identical with a small difference, that's because the results that we compared our study with, contain a chemical reaction which is absent in the reference. These results confirm the validity of the current numerical scheme used.

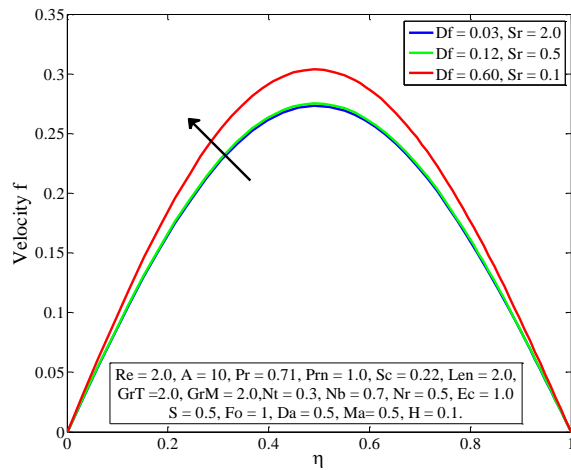


Figure 3. Velocity profile for different values of D_f and S_r

The Figure 3 demonstrates the non-dimensional velocity $f(\eta)$ for different values of the Soret S_r and Dufour D_f numbers. It can be observed from this figure that the fluid velocity increases with the increase of Dufour number D_f (or the decrease the Soret number S_r).

The non-dimensional temperature $\theta(\eta)$ for different values of S_r and D_f numbers is presented in the Figure 4. Here the increase of the fluid temperature leads to the rise of D_f (or the decrease of S_r). Strong thermodiffusion affect f and more in T .

Figure 5 shows the non-dimensional concentration $\phi(\eta)$ for different values of S_r and D_f numbers. From this figure, it can be seen that the fluid concentration diminishes with the

increase of D_f (or the decrease of number S_r).

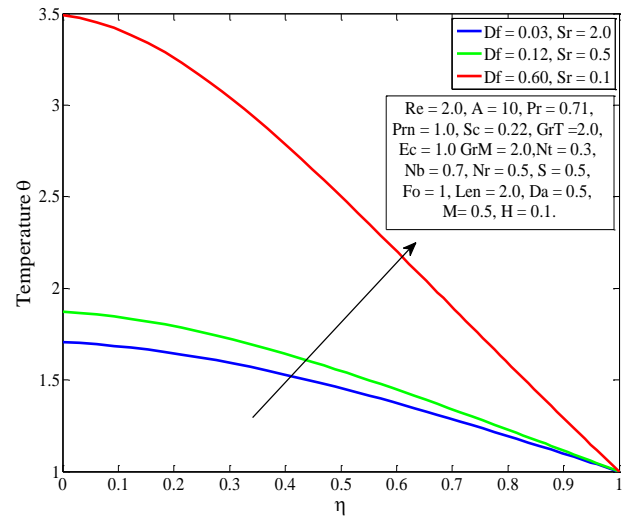


Figure 4. Temperature profile for different values of D_f and S_r

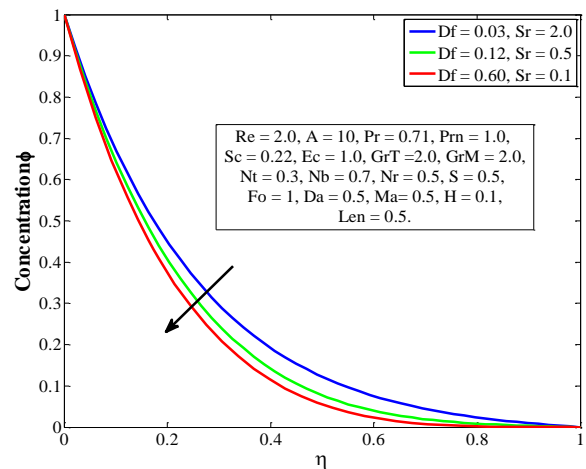


Figure 5. Concentration profile for different values of D_f and S_r

Figure 6 represents the non-dimensional concentration of nanoparticles $\psi(\eta)$ for different values of S_r and D_f numbers. It's observed that the decrease of the nanoparticle's fluid concentration is caused by the augmentation of D_f (or the deceleration of S_r).

Figure 7 shows the effects of Darcy Da and Fo numbers on the velocity profile. As it is demonstrated; the velocity profile decelerates with increasing of Darcy number; meanwhile, the rise in Forchheimer number reduces the velocity profile. Also, as Darcy and Forchheimer numbers decrease, the temperature field declines, such it is illustrated on the Figure 8.

The Figure 9 expresses the concentration profile for different values of Da and Fo numbers. It can be seen that their augmentation causes a little increase in the concentration profile, which expressed that no effect of structural medium on this quantity. The same effect is observed in Figure 10 which represents the non-dimensional concentration of nanoparticles.

In the Figures 11 to 14, the effects of couple stress parameter S and Hartmann number M on the velocity, temperature, concentration and concentration nanoparticles non-dimensional profiles are presented.

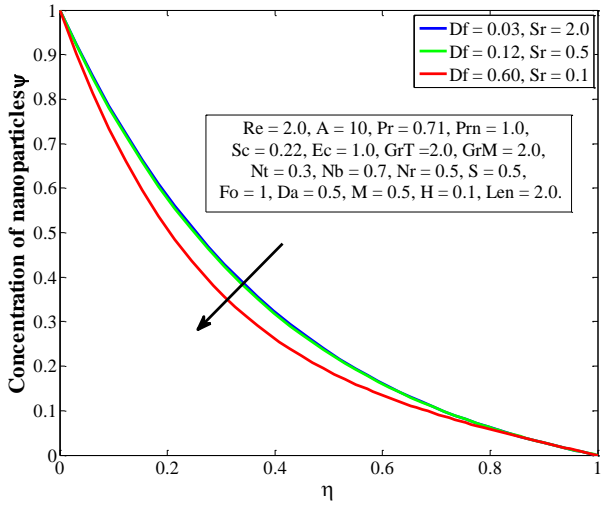


Figure 6. Concentration of nanoparticles profile for different values of D_f and S_r

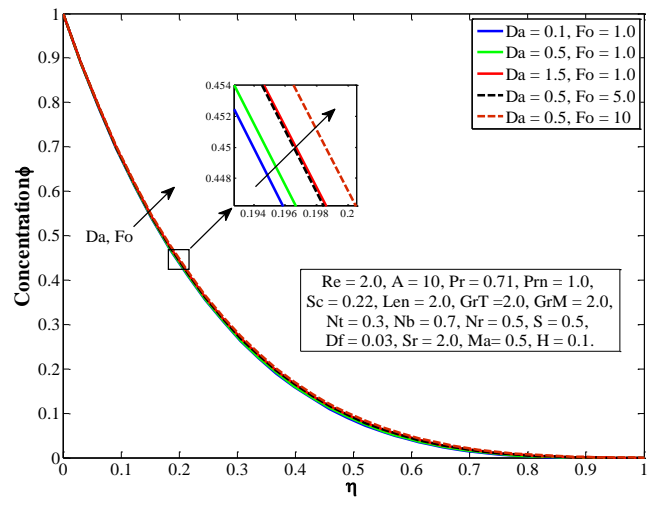


Figure 9. Concentration profile for different values of Da and Fo

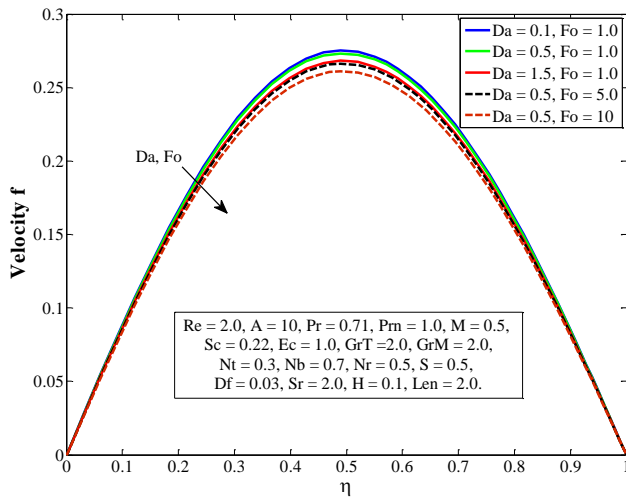


Figure 7. Velocity profile for different values of Da and Fo

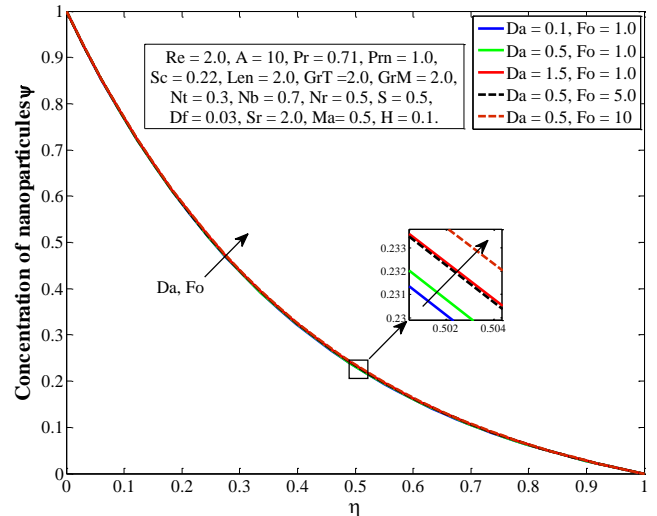


Figure 10. Concentration of nanoparticles profile for different values of Da and Fo

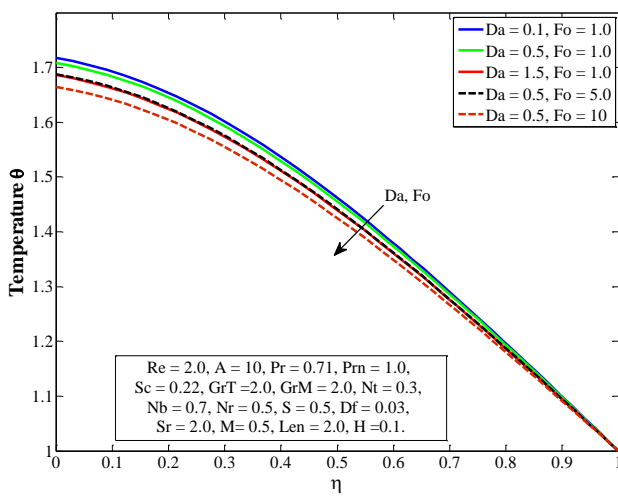


Figure 8. Temperature profile for different values of Da and Fo

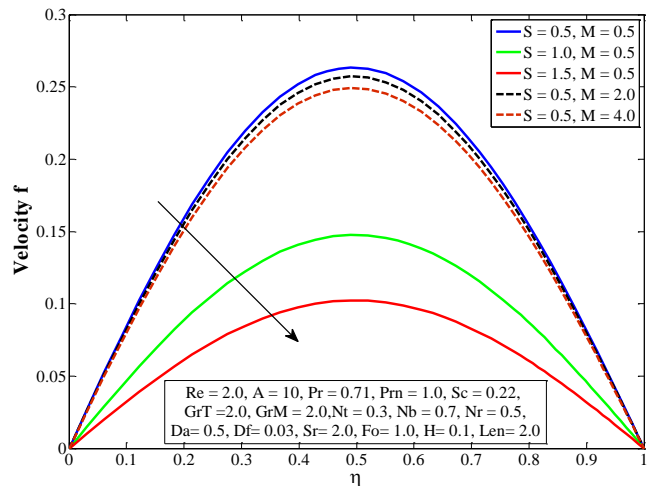


Figure 11. Velocity profile for different values of S and M

It can be observed from Figure 11 that the velocity decreases as S and M increase. In the Figure 12, it can be shown that the temperature decreases also with the increase of couple stress parameter S or number Hartmann number M .

Nevertheless, we observe from the Figures 13 and 14, that the raise of S and M cause a little increase in both of the concentration and the concentration of nanoparticles.

The Figures 15, 16, 17 and 18 demonstrate the effects of thermophoresis Nt and Brownian motion Nb parameters on the velocity $f(\eta)$, the temperature $\theta(\eta)$, the concentration $\phi(\eta)$ and the concentration of nanoparticles $\psi(\eta)$. It can be clearly observed that as Nt and Nb increase, both the velocity and the temperature augment, however the concentration decreases. Moreover, it's shown that as Nt increases, the concentration of nanoparticles profile decreases, and that the concentration of nanoparticles augments when Nb decelerates.

The Figures, from 19 to 22, represent the effects of the thermal Grashof number Gr_T and concentration Grashof number Gr_M on the non-dimensional velocity, the temperature, the concentration and concentration of the nanoparticle's profiles. It is noticed that the raise in each of these parameters cause the augmentation of velocity and temperature profiles.

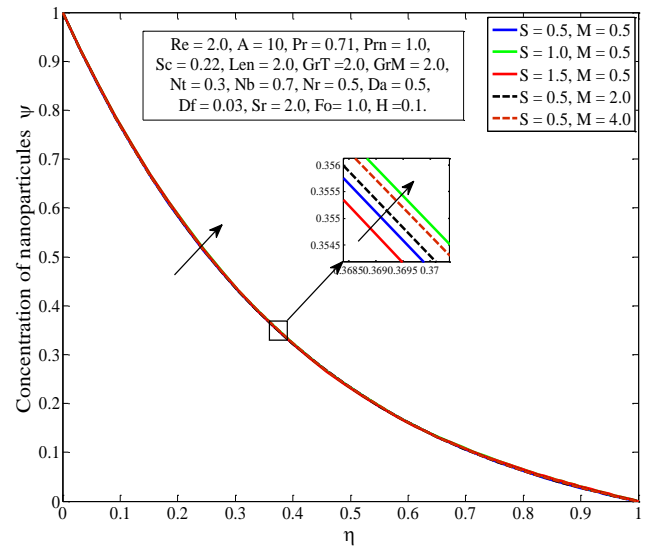


Figure 14. Concentration of nanoparticles profile for different values of S and M

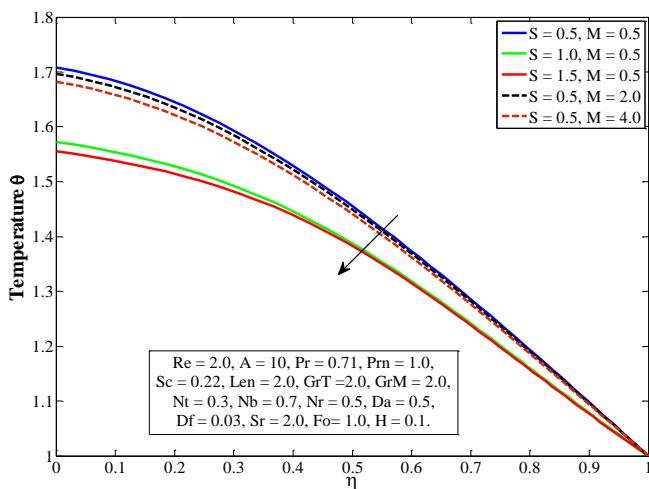


Figure 12. Temperature profile for different values of S and M

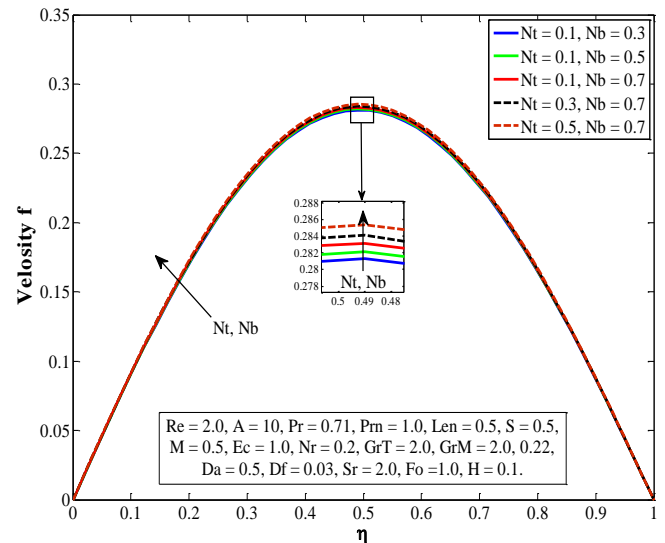


Figure 15. Velocity profile for different values of Nt and Nb

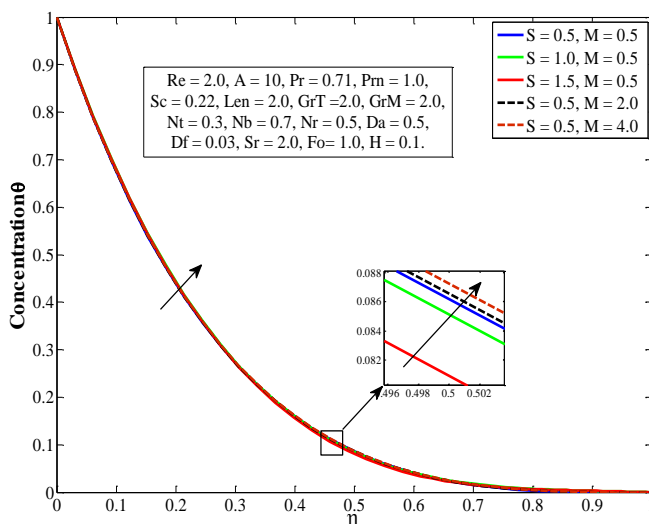


Figure 13. Concentration profile for different values of S and M

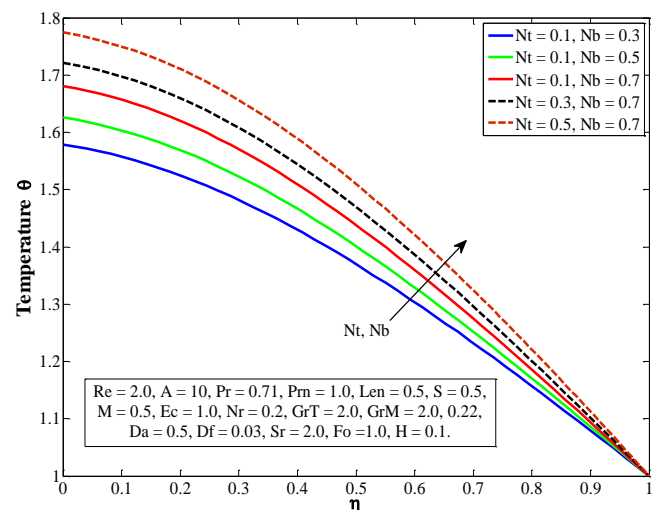


Figure 16. Temperature profile for different values of Nt and Nb

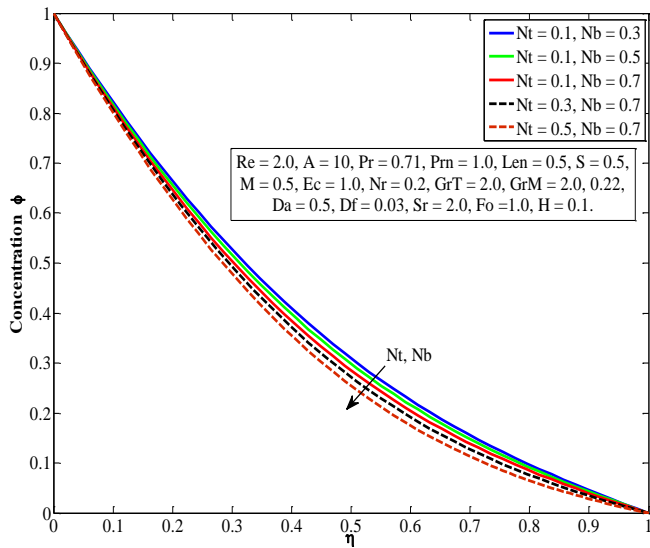


Figure 17. Concentration profile for different values of Nt and Nb

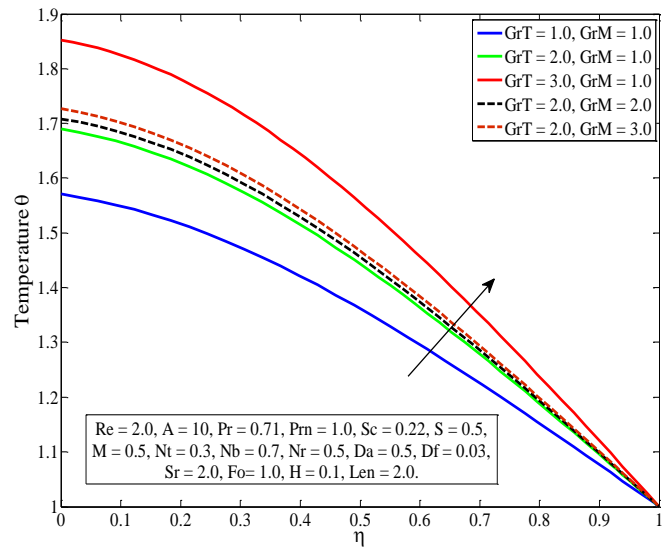


Figure 20. Temperature profile for different values of Gr_T and Gr_M

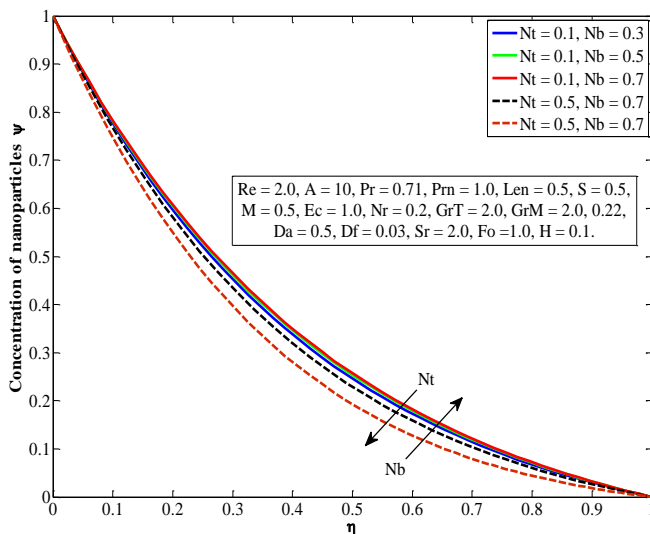


Figure 18. Concentration of nanoparticles profile for different values of Nt and Nb

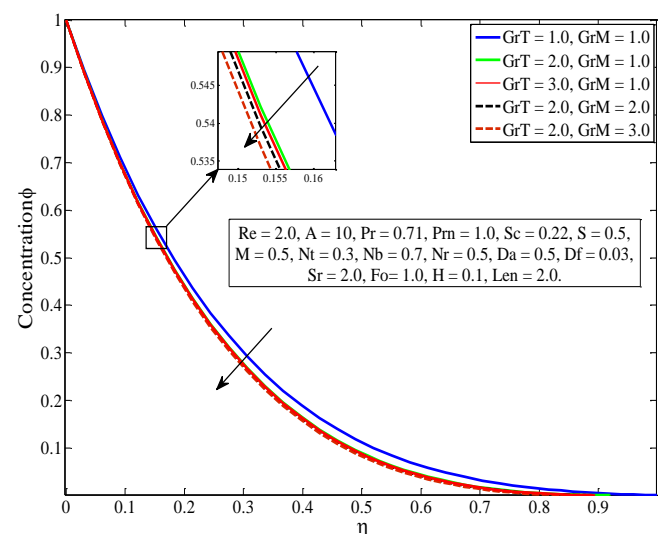


Figure 21. Concentration profile for different values of Gr_T and Gr_M

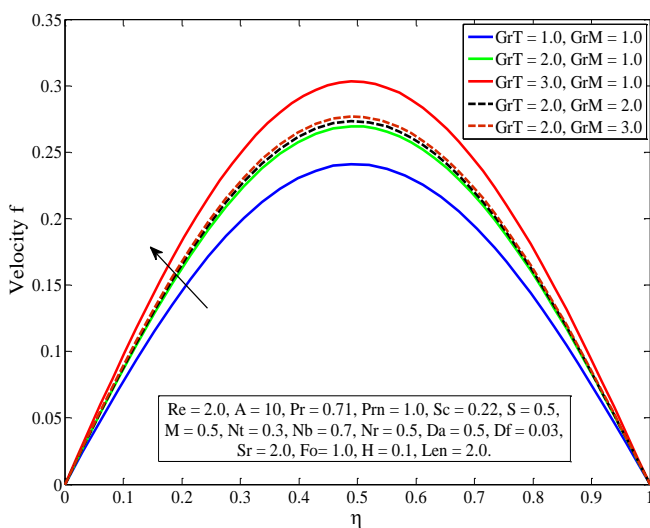


Figure 19. Velocity profile for different values of Gr_T and Gr_M

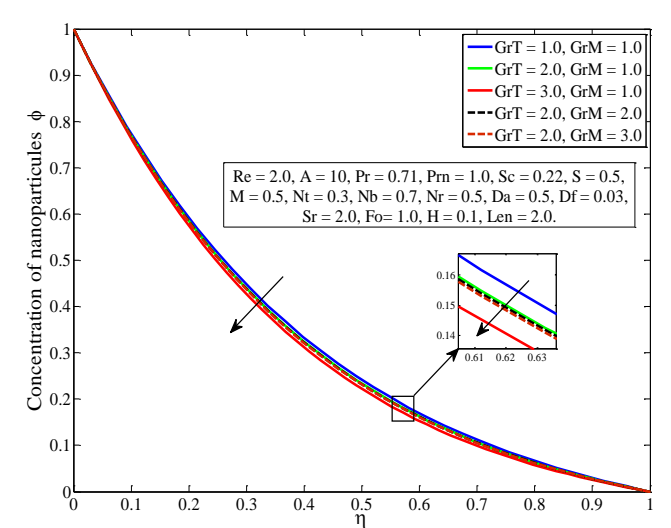


Figure 22. Concentration of nanoparticles profile for different values of Gr_T and Gr_M

The fluid and nanoparticles concentrations for different values of Gr_T , and Gr_M are displayed in the Figure 21 and 22, respectively. It is observed that by increasing Gr_T , and Gr_M , the fluid and the nanoparticles concentrations decelerate.

The Figure 23 demonstrates the non-dimensional velocity for different values of Nanofluid Lewis number Le_n and the nanofluid buoyancy ratio parameter N_r . It is shown, from that figure, that the velocity of the fluid decreases with the increase of Le_n or N_r .

The Figures 24 and 25 express the effects of Le_n and N_r on the temperature and the concentration profiles. It can be seen that as Le_n increases, the temperature increases however the concentration decreases. But for N_r , we observed that as it increases, the temperature decreases and the concentration increases.

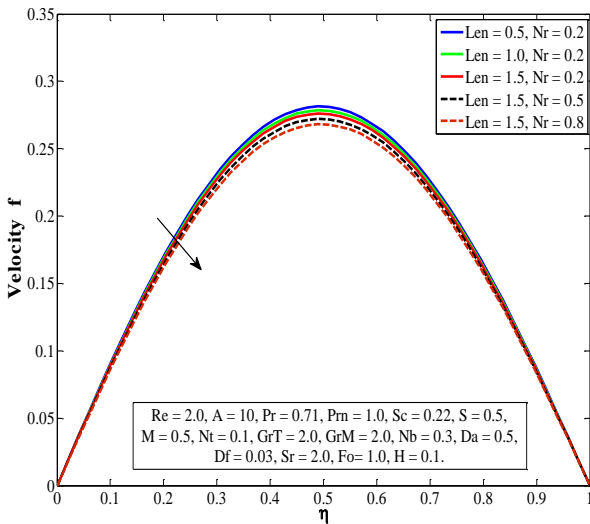


Figure 23. Velocity profile for different values of Le_n and N_r

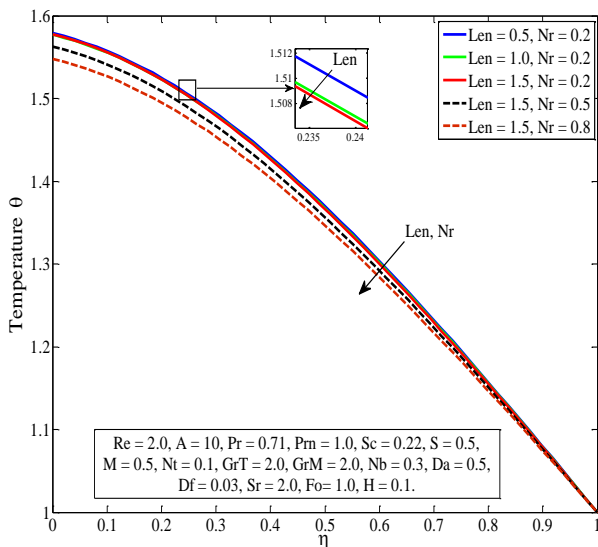


Figure 24. Temperature profile for different values of Le_n and N_r

The Figures 24 and 25 express the effects of Nanofluid Lewis number Le_n and the nanofluid buoyancy ratio parameter N_r on the temperature and the concentration profiles. It can be seen that as Le_n increases, the temperature increases however the concentration decreases. But for N_r , we observed that as it increases, the temperature decreases and the concentration increases.

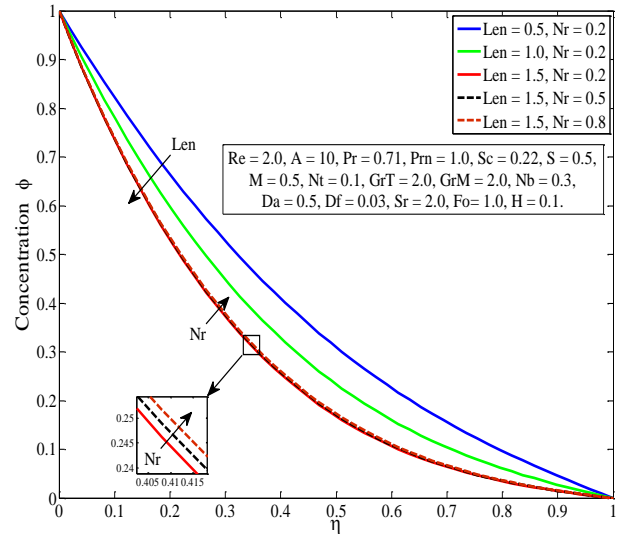


Figure 25. Concentration profile for different values of Le_n and N_r

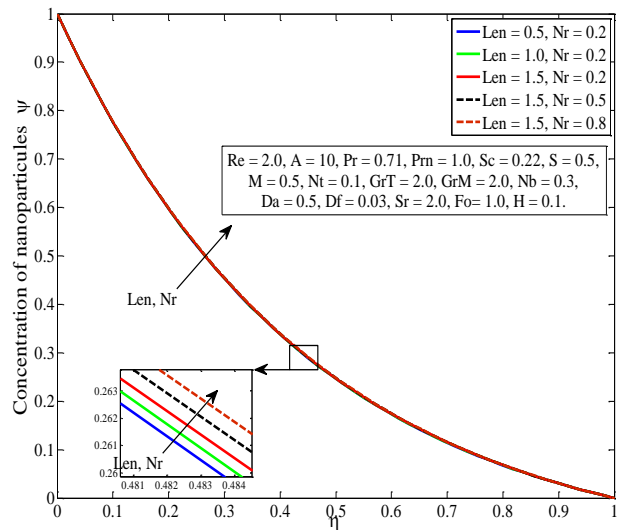


Figure 26. Concentration of nanoparticles profile for different values of Le_n and N_r

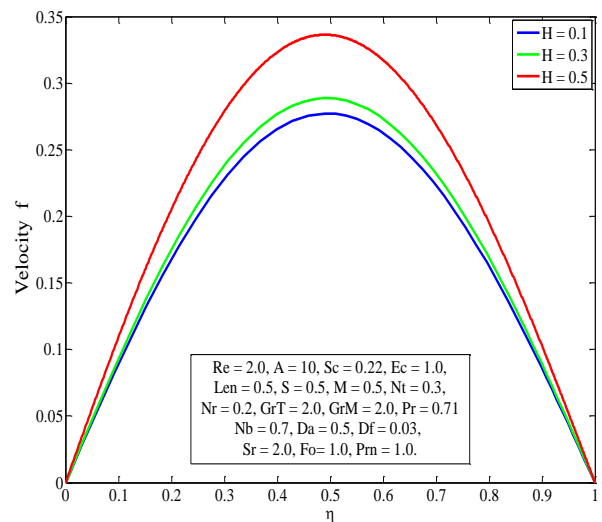


Figure 27. Velocity profile for different values of H

The Figure 26 shows Le_n and N_r effects on the concentration

of nanoparticles profile. It is observed that the concentration of nanoparticles profile rises with increasing both of Le_n and N_r .

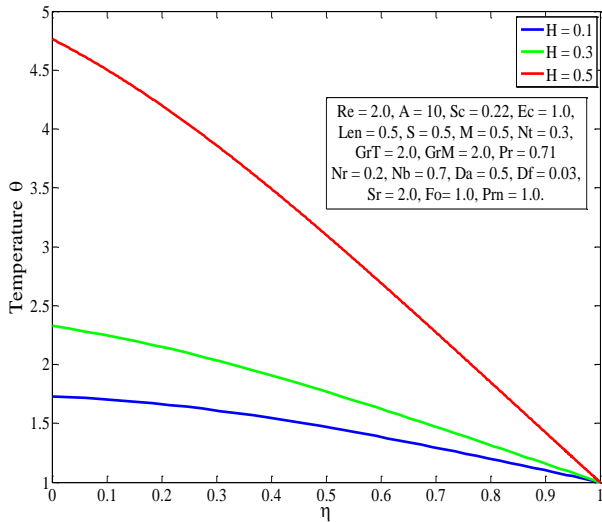


Figure 28. Temperature profile for different values of H

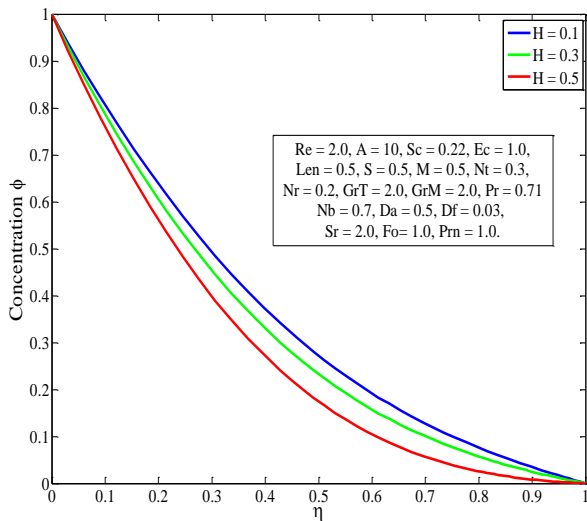


Figure 29. Concentration profile for different values of H

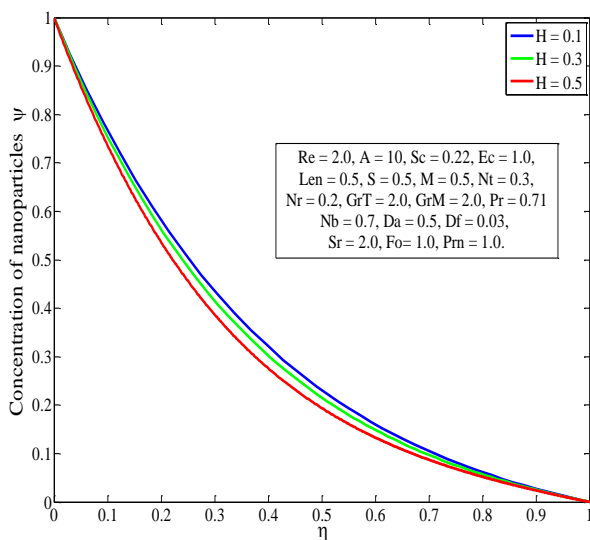


Figure 30. Concentration of nanoparticles profile for different values of H

The Figures 27 and 28 show the non-dimensional velocity and temperature profiles for different values of the Biot number H. From these figures, it can be seen that both of velocity and temperature of the fluid increase with the raise of H, and the augmentation of H causes the diminution of the fluid and the nanoparticles concentrations, as illustrated in the Figures 29 and 30.

Table 1. Values of Nu_x for the selected values of D_f , S_r , S, M and H

D_f	S_r	S	M	H	Nu_1	Nu_2
0.60	0.1	0.5	0.5	0.1	0.1702	0.9991
0.30	0.2				0.1730	1.0297
0.12	0.5				0.1925	1.2593
0.60	0.1	0.5	0.5	0.1	0.1702	0.9991
		1.0			0.1560	0.7689
		1.5			0.1542	0.7393
0.03	2.0	0.5	0.5	0.1	0.1702	0.9991
			2.0		0.1690	0.9797
			4.0		0.1675	0.9549
0.03	2.0	0.5	0.5	0.1	0.1702	0.9991
				0.3	0.6840	1.5382
				0.5	1.6415	2.2973

Table 2. Values of Sh_x for the selected values of D_f , S_r , S, M and H

D_f	S_r	S	M	H	Sh_1	Sh_2
0.03	2.0	0.5	0.5	0.1	2.0328	0.3295
0.12	0.5				2.1165	0.1870
0.60	0.1				2.2606	0.0474
0.03	2.0	0.5	0.5	0.1	2.0328	0.3295
		1.0			1.9438	0.3839
		1.5			1.9406	0.3848
0.03	2.0	0.5	0.5	0.1	2.0328	0.3295
			2.0		2.0240	0.3349
			4.0		2.0124	0.3420
0.03	2.0	0.5	0.5	0.1	2.0328	0.3295
				0.3	2.2637	0.2358
				0.5	2.5963	0.2461

The local Nusselt and Sherwood numbers for different values of D_f , S_r , S, M and H for both plates are presented in the Table 1 and Table 2 respectively. The other parameters values are fixed: $A=10$; $Re = Gr_T = Gr_M = 2.0$; $Pr = 0.71$; $Pr_n = Ec = Fo = 1.0$; $Sc = 0.22$; $Da = Le_n = Nr = 0.5$; $Nb=0.7$; and $Nt=0.3$.

Heat transfer rate is substantially improved with the increasing of S_r or H. A contrary observed effect from Table 1 is with the increase of S at the two walls. On the other hand, Table 1 shows that M is without effect on the Nusselt numbers. Interesting result is that the Dufour number plays a reverse role in relation to the Soret effect.

The mass transfer rate diminishes at the initial plate $y=-d$ and increases while this rate augments largely at the terminal $y=d$ when Soret number S_r increases or Dufour number D_f decreases. However, no perceptible effect is revealed with the variations of S, the Hartmann M and Biot H numbers for high values of these parameters.

4. CONCLUSION

Magnetohydrodynamic MHD flow of couple stress

nanoparticles between two parallel walls packed with a saturated porous medium with heat and mass transfer was investigated in this study considering a great number impacting on the physical system. Similarity transformations are used for the nonlinear and highly coupled partial differential equations resulting from the complex model. The governing non-dimensional differential equations are numerically solved using the finite differences method with the Lobatto III's scheme. The computational results are presented through figures respecting effects of D_f , S_r , Da , Fo , S , M , Nb , Nt , Nr , Le_n , Gr_T , Gr_M , H on the velocity, temperature, concentration and the concentration of nanoparticles profiles..

The main observations of the present analysis are listed below:

- The Soret and Dufour effects have a great importance and cannot neglected for some specific values because they can change largely the velocity and temperature profiles. Particularly, they affect strongly the heat transfer and mass transfer rates at specific walls.
- The structural porous medium via the Darcy and Forshheimer numbers have no perceptible impact on all the profiles. This is also valuable to a couple stress nanofluid in all ranges of the Lewis number.
- The level of the couple stress fluid as well as the magnetic field imposed can substantially modified the velocity and temperature profiles but less effect on the heat and mass rates.
- The use of a nanofluid combined with a couple stress lead strictly to act on the temperature profile.
- A physical channel and thermal system with a convective heat condition at the wall is more affected compared with a system conducted by a constant temperature at the boundary.

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NOMENCLATURE

u, v	Velocity component along x and y directions, respectively.
x, y	Cartesian coordinates along the plate and normal to it.
T	Temperature
C	Concentration
P	Pressure
g	Gravitational acceleration
B_0	Externally imposed magnetic field in the y direction
D_B	Brownian diffusion coefficient
D_T	Thermophoresis diffusion coefficient
D_m	Molecular solutal diffusivity
K_T	Thermal diffusion ratio
T_m	Mean fluid temperature
K	Porous medium parameter
C_S	Concentration susceptibility
h_f	Heat transfer coefficient
f	Dimensionless velocity
A	pressure gradient
Re	Reynolds number
S	Couple stress parameter
Gr_T	Thermal Grashof number
Gr_M	Concentration Grashof number
Nr	Nanofluid buoyancy ratio parameter
M	Hartmann number
Da	Darcy number
Fo	Forchheimer number
Pr	Prandtl number
Ec	Eckert number
Nb	Brownian motion parameter
Nt	thermophoresis parameter
D_f	Dufour number
S_r	Soret Number
Le_n	Thermo-nanofluid Lewis number
Pr_n	Prandtl nanofluid number
H	Biot number
Nu	Local Nusselt number
Sh	Local Sherwood number

Greek symbols

ϕ	Nanoparticles concentration
μ	Dynamic viscosity
ρ_f	Density of the fluid

ρ_p	Density of nanoparticle	$(\rho C_p)_p$	Heat capacity of nanoparticles
η	Couple stress viscosity parameter	α_f	Thermal diffusivity
β_T	Thermal expansion coefficient	ε	Porosity
β_C	Concentration expansion coefficient	η	Similarity variable
σ	Electrical conductivity	θ	Dimensionless temperature
c_f	Forchheimer constant	φ	Dimensionless concentration
λ	Thermal conductivity	ψ	Dimensionless concentration of nanoparticles
$(\rho C_p)_f$	Heat capacity at constant pressure of fluid		