

EFFECTS OF VARIABLE VISCOSITY AND THERMAL CONDUCTIVITY ON THE MHD FLOW OF MICROPOLAR FLUID PAST AN ACCELERATED INFINITE VERTICAL INSULATED PLATE

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ABSTRACT

The effects of temperature dependent viscosity and thermal conductivity on magneto hydrodynamic flow, heat and mass transfer of an incompressible micropolar fluid past an accelerated infinite vertical plate are studied where the viscosity and thermal conductivity are assumed to be inverse linear functions of temperature. The partial differential equations governing the flow, heat and mass transfer of the problem are transformed into dimensionless form of ordinary differential equations by using similarity substitutions. The governing boundary value problems are then solved numerically using shooting method. The effects of various parameters viz. viscosity parameter, thermal conductivity parameter, mass transfer parameter, coupling constant parameter, Prandtl number, Schmidt number, Reynolds number and magnetic parameter on velocity, micro-rotation, temperature and concentration fields are obtained and presented graphically. The Skin-friction, Nusselt number and Sherwood number are also computed and presented in tabular form.

Keywords: Micropolar fluid, Variable viscosity and thermal conductivity, Mass transfer, MHD Flow.

1. INTRODUCTION

The theory of micropolar fluid has been a field of very active research for the last few decades. This theory, first introduced and formulated by Eringen [4] (1966), is capable to explain the complex fluids behaviour such as liquid crystals, polymeric suspensions, animal blood etc. by taking into account the effect arising from local structure and micro-motions of the fluid elements. In the theory of micropolar fluid, each particle has a finite size and constitutes a micro structure, which can rotate. This local rotation of the particles is in addition to the usual rigid body motion of the entire volume element. The effect of magneto hydrodynamics on micropolar flow has become important due to several engineering applications such as in MHD generators, designing cooling system for nuclear reactor, flow meters etc., where the micro concentration provides an important parameter for deciding the rate of heat flow. Several investigators have made theoretical and experimental studies of micropolar flow in the presence of a transverse magnetic field during the last decades. Assuming fluid viscosity as a linear function of temperature the effect of variable viscosity on MHD natural convection in micropolar fluids was studied by Abd El-Hakim *et al.* [1]. Ahmed and Kalita [2] studied MHD oscillatory free convective flow past a vertical plate in slip- flow regime with variable suction and periodic plate temperature. MHD free and forced convection and mass transfer flow past a porous vertical plate was investigated by Ahmed and Hazarika [3]. Gorla *et al.* [5] investigated the magneto hydrodynamic free convection boundary layer flow of a thermomicropolar fluid over a vertical plate.

Muthucumaraswami *et al.* [8] investigated the unsteady flow past an accelerated infinite vertical plate with variable temperature and uniform mass diffusion. Rajesh [9] investigated the MHD free convection flow past an accelerated vertical porous plate with variable temperature through a porous medium. Using similarity substitutions and applying shooting method Sarma and Hazarika [10] investigated effects of variable viscosity and thermal conductivity on the flow of Newtonian fluid past an accelerated vertical insulated plate.

2. OBJECTIVE

The main objective of the present work is to extend the work of Sarma and Hazarika [10] for the study of the effects of variable viscosity and thermal conductivity on the MHD flow of micropolar fluid past an accelerated infinite vertical insulated plate. Viscosity and thermal conductivity are assumed to be inverse linear functions of temperature. The governing partial differential equations are reduced in to ordinary differential equations by similarity transformations. The problem is then solved numerically using Runge-Kutta shooting algorithm.

3. MATHEMATICAL FORMULATION OF THE PROBLEM

The general equations of fluid motion for two dimensional unsteady flows in Cartesian co-ordinate are considered

with x –axis along the vertical plate in the upward direction and the y –axis normal to it, where the fluid properties, viscosity, thermal conductivity and concentration are assumed to vary with temperature. At time $t>0$ the infinite plate starts moving with a velocity $u = c_0 t$ (where c_0 is a positive constant with the dimension of acceleration). As the velocity of the fluid is low, so the viscous dissipative heat is neglected. Also a magnetic field of constant intensity is assumed to be applied normal to the vertical plate and the electrical conductivity of the fluid is assumed to be so small that the induced magnetic field can be neglected in comparison to the applied magnetic field. The applied magnetic field is primary in the y –direction and is a function of t only. $(u(y, t), 0)$ are the velocity components and N is the component of micro-rotation perpendicular to the xy – plane. Under these assumptions the governing equations of the problem are considered as follows:

3.1 Governing equations

Momentum equation:

$$\frac{\partial u}{\partial t} = g_0 \beta (T - T_\infty) + g_0 \beta^* (C - C_\infty) + \frac{\partial}{\partial y} \left(\nu \frac{\partial u}{\partial y} \right) + \frac{\kappa}{\rho} \left(\frac{\partial N}{\partial y} + \frac{\partial^2 u}{\partial y^2} \right) - \frac{\sigma B^2}{\rho} u \quad (1)$$

Angular momentum equation:

$$\frac{\partial N}{\partial t} = \frac{\gamma}{\rho j} \frac{\partial^2 N}{\partial y^2} - \frac{\kappa}{\rho j} (2N + \frac{\partial u}{\partial y}) \quad (2)$$

Energy equation:

$$\frac{\partial T}{\partial t} = \frac{1}{\rho c_p} \frac{\partial}{\partial y} \left(\lambda \frac{\partial T}{\partial y} \right) \quad (3)$$

Species continuity equation:

$$\frac{\partial C}{\partial t} = \frac{1}{s_c} \frac{\partial}{\partial y} \left(\nu \frac{\partial C}{\partial y} \right) \quad (4)$$

3.2 Boundary conditions

The appropriate boundary conditions are:

$$\left. \begin{aligned} u(0, t) = 0, T(0, t) = T_w, C(0, t) = C_w, N(0, t) = 0, \\ u(\infty, t) = 0, T(\infty, t) = 0, C(\infty, t) = 0, N(\infty, t) = 0 \end{aligned} \right\} \quad (5)$$

The equation of continuity being identically satisfied by $(u(y, t), 0)$. Following Gurum [6] we assume that $\gamma = \left(\mu_\infty + \frac{\kappa}{2} \right) j = \mu_\infty \left(1 + \frac{K_1}{2} \right) j$, where $K_1 = \frac{\kappa}{\nu_\infty \rho}$, coupling constant parameter.

Following Lai and Kulacki [7] we assume that the viscosity and thermal conductivity are inverse linear functions of temperature, i.e.

$$\frac{1}{\mu} = \frac{1}{\mu_\infty} [1 + \delta(T - T_\infty)], \text{ or } \frac{1}{\mu} = a(T - T_c)$$

$$\text{where } a = \frac{\delta}{\mu_\infty} \text{ and } T_c = T_\infty - \frac{1}{\delta}$$

$$\frac{1}{\lambda} = \frac{1}{\lambda_\infty} [1 + \xi(T - T_\infty)], \text{ or } \frac{1}{\lambda} = b(T - T_r)$$

$$\text{Where } b = \frac{\xi}{\lambda_\infty} \text{ and } T_r = T_\infty - \frac{1}{\xi}$$

Here a, b, T_c and T_r are constants and their values depend on the reference state and thermal properties of the fluid i.e. ν and λ . In general $a, b > 0$ for liquids and $a, b < 0$ for gases.

We introduce the following similarity transformations:

$$\eta = y \sqrt{\frac{\alpha^2 U_0}{(1 - \alpha t) \nu_\infty c_0}}$$

$$u = U_0 (1 - \alpha t)^{1/2} f(\eta),$$

$$N = \sqrt{\frac{U_0^3 \alpha^2}{\nu_\infty c_0}} h(\eta),$$

$$j = \frac{\nu_\infty c_0}{U_0 \alpha^2} (1 - \alpha t) i(\eta),$$

$$B = \sqrt{\frac{\alpha U_0}{c_0 (1 - \alpha t)}} B_0,$$

$$C = C_\infty + \frac{c_0 (C_w - C_\infty)}{\alpha U_0} (1 - \alpha t)^{1/2} g(\eta),$$

$$T = T_\infty + \frac{c_0 (T_w - T_\infty)}{\alpha U_0} (1 - \alpha t)^{1/2} \theta(\eta),$$

$$G_r = \frac{g_0 \beta (T_w - T_\infty) c_0^2 (1 - \alpha t)}{U_0^3 \alpha^3}, \quad G_c = \frac{g_0 \beta^* (C_w - C_\infty) c_0^2 (1 - \alpha t)}{U_0^3 \alpha^3}.$$

Introducing the above transformations in equations (1)–(4), we have the following non dimensional ordinary differential equations

$$\left(1 + K_1 \frac{\theta_c - \theta}{\theta_c} \right) f'' = \left[G_r \theta + G_c g + K_1 h' - M f - \frac{1}{2} K_2 R_e (f - \eta f') \right] \frac{\theta - \theta_c}{\theta_c} + \frac{\theta' f'}{\theta - \theta_c} \quad (6)$$

$$(2 + K_1) i h'' = K_2 R_e (\eta h') i + K_1 (4h + 2f') \quad (7)$$

$$\theta'' = \frac{1}{2} K_2 P_{e_h} (\theta - \eta \theta') \frac{\theta - \theta_r}{\theta_r} + \frac{\theta'^2}{\theta - \theta_r} \quad (8)$$

$$g'' = \frac{1}{2} K_2 P_{e_m} (g - \eta g') \frac{\theta - \theta_c}{\theta_c} + \frac{g' \theta'}{\theta - \theta_c} \quad (9)$$

The boundary conditions (5) become

$$\left. \begin{aligned} \text{As } \eta = 0: f = 0, g = 1, \theta = 1, h = 0 \\ \text{As } \eta \rightarrow \infty: f = 0, g = 0, \theta = 0, h = 0 \end{aligned} \right\} \quad (10)$$

The physical quantities of interest in this problem are the skin–friction coefficient c_f , Nusselt number Nu and Sherwood number S_h which indicate physically wall shear stress, rate of heat transfer and rate of mass transfer

respectively. For micropolar boundary layer flow, the wall shear stress τ_w is given by

$$\tau_w = \left[(\mu + k) \frac{\partial u}{\partial y} + kN \right]_{y=0}$$

$$= \rho \nu_\infty \left(\frac{\theta_c}{\theta_c - 1} + K_1 \right) \sqrt{\frac{U_0^3 \alpha^2}{\nu_\infty c_0}} f'(0)$$

The skin friction coefficient c_f can be defined as

$$c_f = \frac{2\tau_w}{\rho U_0^2} = 2 \left(\frac{\theta_c}{\theta_c - 1} + K_1 \right) Re^{-\frac{1}{2}} f'(0)$$

The heat transfer from the plate is given by

$$q_w = -\lambda \left[\frac{\partial T}{\partial y} \right]_{y=0} = \lambda_\infty \frac{\theta_r}{1 - \theta_r} \sqrt{\frac{U_0 c_0}{\nu_\infty \alpha^2}} \frac{(T_w - T_\infty) \alpha}{U_0} \theta'(0)$$

The Nusselt number is given by

$$Nu = \frac{q_w U_0}{\lambda_\infty (T_w - T_\infty) \alpha} = \frac{\theta_r}{1 - \theta_r} Re^{\frac{1}{2}} \theta'(0)$$

The mass flux at the wall is given by

$$M_w = -D \left[\frac{\partial C}{\partial y} \right]_{y=0} = -\frac{\nu}{Sc} \sqrt{\frac{U_0 c_0}{\nu_\infty \alpha^2}} \frac{(C_w - C_\infty) \alpha}{U_0} g'(0)$$

$$Sh = \frac{Sc M_w U_0}{\nu_\infty (C_w - C_\infty) \alpha} = \frac{\theta_c}{1 - \theta_c} Re^{\frac{1}{2}} g'(0)$$

4. RESULTS AND DISCUSSION

4.1 Discussion

The equations (6)-(9) together with the boundary conditions (10) are solved for various combinations of the parameters involved in the equations using an algorithm based on the shooting method and results are displayed in the form graph for the dimensionless velocity distribution, dimensionless micro-rotation distribution, dimensionless species concentration distribution, dimensionless temperature distribution with the variation of different parameters.

The values of different parameters have been taken as $Re = 0.10$, $G_r = 0.10$, $G_c = 0.10$, $M = 1$, $Pr = 0.70$, $Sc = 1$, $K_1 = 0.10$, $K_2 = 0.10$ with the viscosity parameter θ_c ranging from -10 to -1 at certain value of $\theta_r = -10$ unless otherwise stated. Similarly solutions have been found with the thermal conductivity parameter θ_r ranging from -15.00 to -1.00 at certain value of $\theta_c = -10.00$ keeping the other values remaining same. Solutions have also been found for different values of magnetic parameter (M), Prandtl number (Pr), Reynolds number (Re), coupling constant parameter (K_1) and Schmidt number (Sc). The variations in velocity distribution, micro-rotation distribution, species concentration distribution and temperature distribution are illustrated in figures (1)–(14) with the variation of different parameters.

The figures (1)–(6) represent the variations in dimensionless velocity distribution with the variation of dimensionless reference temperature corresponding to viscosity parameter θ_c , dimensionless reference temperature

corresponding to thermal conductivity parameter θ_r , Reynolds number Re , the coupling constant parameter K_1 , magnetic parameter M and Schmidt number Sc . From figure (1) it is clear that velocity increases with the increasing values θ_c . This is due to the fact that when the temperature increases viscosity decreases and therefore velocity increases. From figure (2) it is observed that velocity decreases with the increasing values of θ_r . It is due to the reason that temperature decreases with the increasing values of thermal conductivity and as a result viscosity increases and velocity decreases. Figure (3) represents the distribution of velocity with the variation of Reynolds number Re . For small values of Re viscous force is predominant to inertia force and for increasing values of Re viscous force will be decreasing and as a result velocity increases. From figure (4) it is found that velocity decreases with increasing value of coupling constant parameter K_1 . For increasing values of this parameter vortex viscosity increases and therefore velocity decreases. From figure (5) we have observed that velocity decreases with the increasing value of magnetic parameter M . It is due to the fact that the application of transverse magnetic field will result a resistive force (Lorentz force) similar to drag force, which tends to resist the fluid flow and thus reducing its velocity. It is also observed that the velocity is maximum near the plate and decreases away from the plate and finally takes asymptotic value. As the viscosity increases with the increasing values of Schmidt number, from figure (6) we have observed that velocity decreases with the increasing values of Schmidt number.

Figures (7)–(10) display the distributions representing micro-rotation within the boundary layer with the variation of θ_r , θ_c , K_1 and M . From these figures we have observed that the micro-rotation near the surface increases for increasing values of the different parameters and then decreases gradually. It is to be observed that at certain point the parameters have no effect on the micro-rotation distribution. The effect of the Hartmann number M on micro-rotation is shown in the figure (10). The values of micro-rotation are negative in the first half whereas in the second half these are positive, thus showing a reverse rotation nears the boundary. An increase in magnetic field leads to a decrease in micro-rotation.

Figures (11) and (12) display the variations of dimensionless temperature profile $\theta(\eta)$ with the variation of dimensionless reference temperature corresponding to thermal conductivity parameter θ_r and Prandtl number Pr . From figure (11) we have observed that temperature decreases when θ_r increases. It is due to the fact that the kinematic viscosity of the fluid increases with the increase of θ_r and as a result temperature decreases. It is observed from the figure (12) that temperature increases with the increasing values of Pr . It is due to the reason that with the increasing values of the Prandtl number the thermal diffusivity of the fluid decreases and as a result thermal conductivity decreases. Therefore, the volumetric heat capacity of the fluid becomes larger.

Figures (13) and (14) display the distributions representing concentration profile within the boundary layer with the variation of Sc and Re . It is observed that concentration increases with the increasing values of Sc and Re . With the increasing value of Sc mass diffusivity decreases and as a result concentration increases.

4.2 Figures

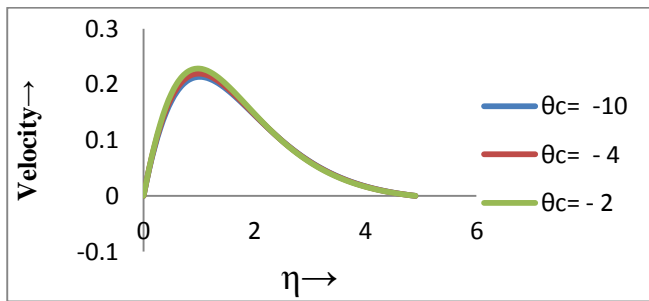


Figure 1. Velocity distribution with the variation of θ_c

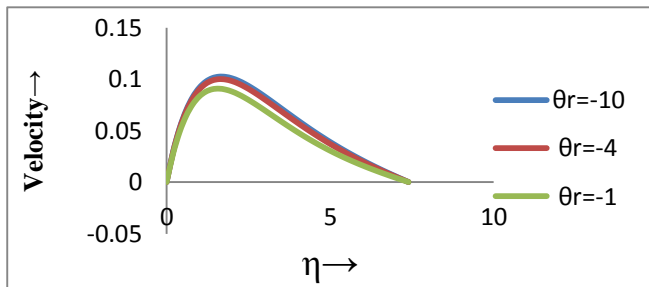


Figure 2. Velocity distribution with the variation of θ_r

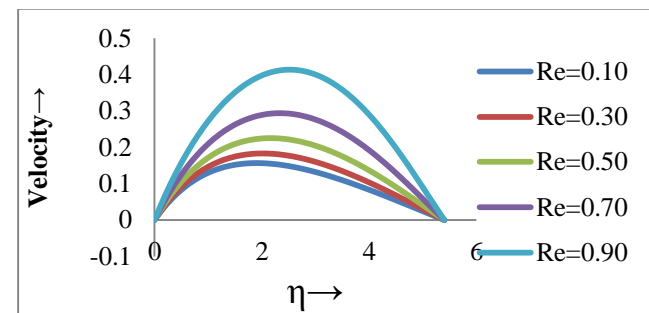


Figure 3. Velocity distribution with the variation of Re

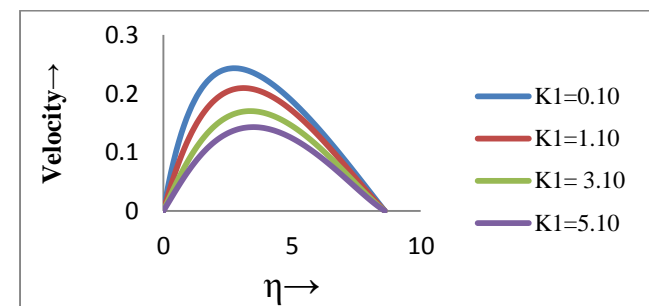


Figure 4. Velocity distribution with the variation of K_1

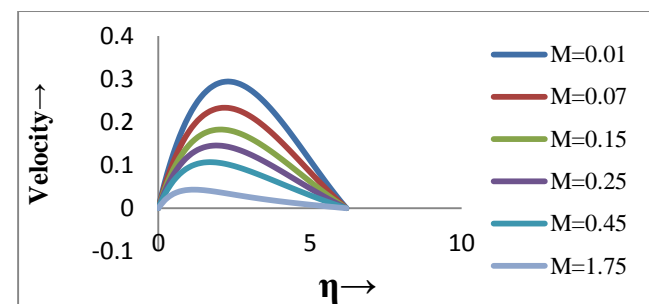


Figure 5. Velocity distribution with the variation of M

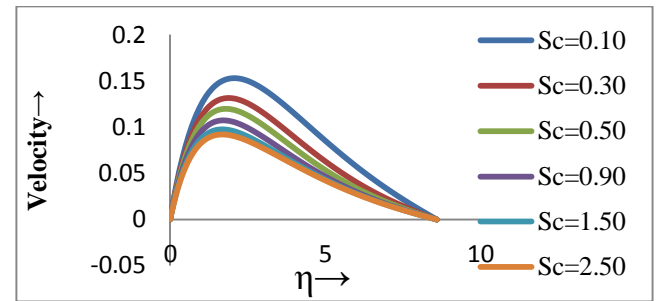


Figure 6. Velocity distributions with the variation of Sc

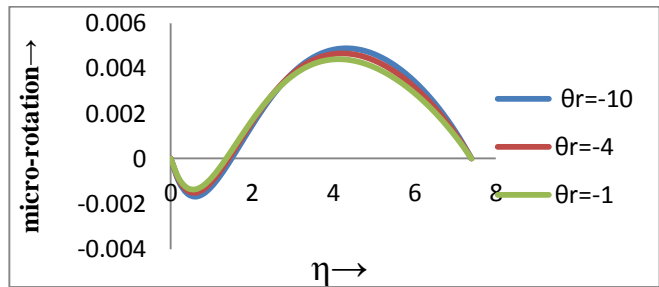


Figure 7. Micro-rotation distribution with the variation of θ_r

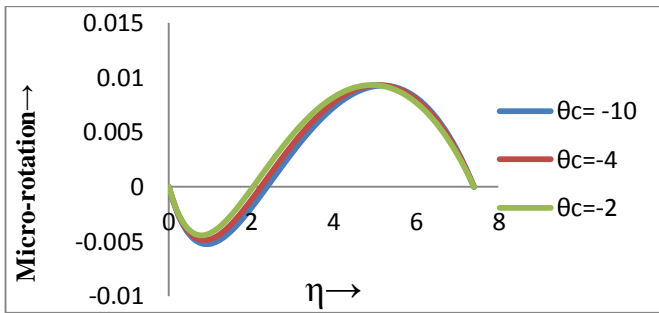


Figure 8. Micro-rotation distributions with the variation of θ_c

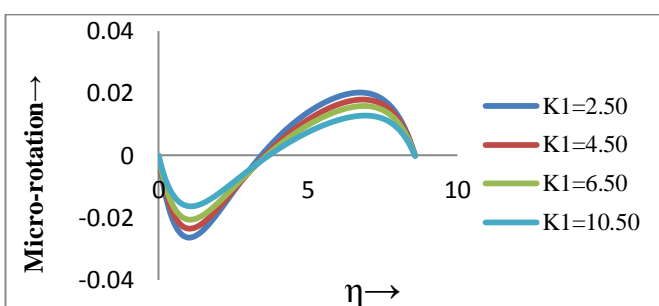


Figure 9. Micro-rotation distribution with the variation of K_1

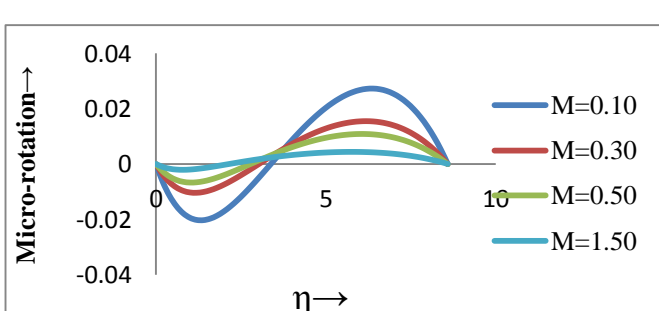


Figure 10. Micro-rotation distribution with variation of M

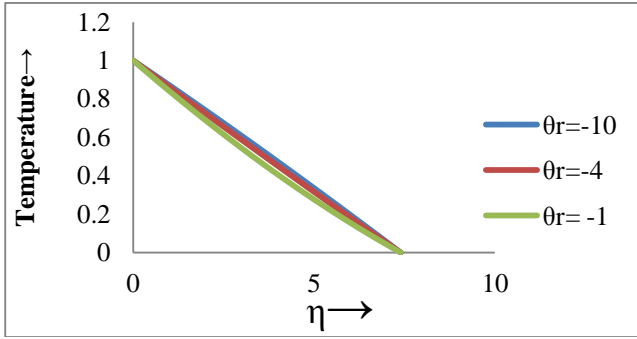


Figure 11. Temperature distribution with the variation of θ_r .

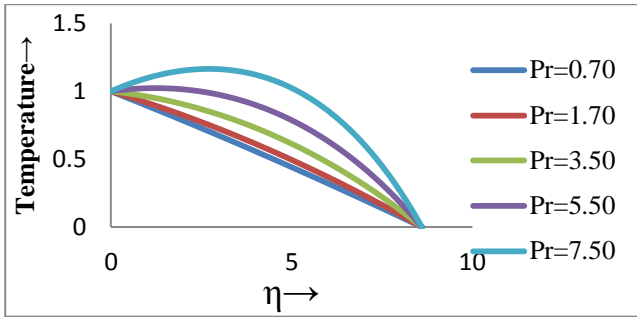


Figure 12. Temperature distribution with the variation of P_r .

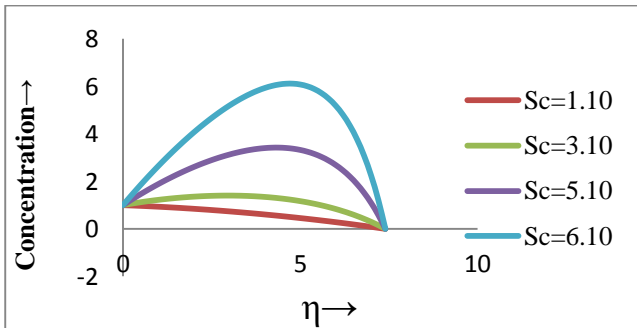


Figure 13. Concentration distribution with the variation of Sc

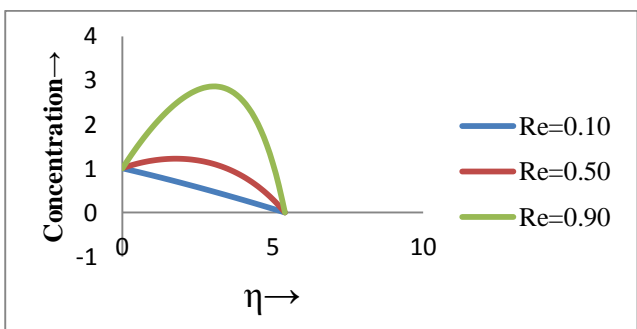


Figure 14. Concentration distribution with the variation of Re

4.3 Numerical values and tables

Finally effects of the above mentioned parameters on the values of $f'(0)$, $g'(0)$, $h'(0)$, $\theta'(0)$, c_f , Nu and S_h are shown in the tables (1)–(4). The behaviours of these parameters are self evident from the tables and hence any further discussions about them are seemed to be redundant.

Table 1. Variations with respect to M and θ_c

M	θ_c	$f'(0)$	$g'(0)$	$h'(0)$	c_f	S_h
0.1	-10	0.38813	-0.0655	-0.0289	2.47707	0.01882
2.1	-5	0.13229	-0.0854	-0.0046	0.78094	0.02251
4.1	-3	0.10135	-0.1119	-0.0025	0.54484	0.02654
6.1	-1	0.09927	-0.2177	-0.0017	0.37671	0.03442

Table 2. Variations with respect to M and θ_r

M	θ_r	$f'(0)$	$g'(0)$	$\theta'(0)$	c_f	Nu	S_h
0.1	-10	0.3881	-0.0655	-0.1273	2.477	0.0365	0.0188
2.1	-5	0.1273	-0.0657	-0.1322	0.812	0.0348	0.0189
4.1	-3	0.0931	-0.0660	-0.1383	0.594	0.0328	0.0190
6.1	-1	0.0768	-0.0673	-0.1623	0.490	0.0256	0.0193

Table 3. Variations with respect to M and P_r

Pr	M	$f'(0)$	$g'(0)$	$\theta'(0)$	c_f	Nu	S_h
0.7	0.1	0.3881	-0.0655	-0.127	2.4770	0.036596	0.018829
3.7	0.3	0.2973	-0.06206	-0.059	1.897	0.01705	0.017841
7.2	0.5	0.2579	-0.05646	0.036	1.6464	-0.01058	0.016231

Table 4. Variations with respect to P_r and θ_r

Pr	θ_r	$f'(0)$	$g'(0)$	$\theta'(0)$	c_f	Nu	S_h
0.7	-10	0.2363	-0.065	-0.1273	1.5086	0.0365	0.018829
6.2	-5	0.2547	-0.058	0.0159	1.6257	-0.004	0.016714
6.7	-3	0.2587	-0.056	0.0481	1.6513	-0.011	0.016323
7.2	-1	0.2811	-0.049	0.2056	1.7943	-0.032	0.014155

5. CONCLUSION

In this study, the effects of variable viscosity and thermal conductivity on the flow with heat and mass transfer of an incompressible micropolar fluid past an accelerated infinite vertical insulated plate are examined. The results demonstrate clearly that the viscosity and thermal conductivity parameters along with the other parameters such as K_1 , Sc , Re , M and P_r have significant effects on velocity, temperature, concentration and micro-rotation distributions within the boundary layer. Thus presence of microconstituents may cause a significant change in flow problem.

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NOMENCLATURES

- α = Measure of unsteadiness with dimension reciprocal to time
- β = Volumetric coefficient of thermal expansion (K^{-1})
- β^* = Volumetric co-efficient of expansion with concentration
- γ = Spin-gradient or micro rotation viscosity
- η = Dimensionless co-ordinates
- λ = Thermal conductivity ($m \cdot kg \cdot s^{-3} \cdot K^{-1}$)
- λ_∞ = Thermal conductivity of the ambient fluid
- μ = Dynamic viscosity (Newton-sec/ m^2)
- μ_∞ = Dynamic viscosity of the ambient fluid
- ν = Kinematic viscosity (Metre²/sec)
- ν_∞ = Kinematic Viscosity of the ambient fluid
- κ = Vortex viscosity
- σ = Electrical conductivity
- ρ = Density ($kg. /m^3$)
- θ = Dimensionless temperature
- θ_c = Dimensionless reference temperature corresponding to viscosity parameter
- θ_r = Dimensionless reference temperature corresponding to thermal conductivity parameter
- g_0 = Gravitational acceleration (m/s^2)

- c_p = Specific heat (J/kg. $^{\circ}C$)
- u = Velocity in the x - direction(m/s)
- f = Dimensionless velocity
- h = Dimensionless microrotation
- g = Dimensionless species concentration
- T = Temperature (Kelvin)
- C = Species concentration ($kg. /m^3$)
- T_∞ = Ambient temperature (Kelvin)
- T_w = Wall temperature (Kelvin)
- C_w = Species concentration at the wall ($kg. /m^3$)
- C_∞ = Species concentration far from the wall ($kg. /m^3$)
- U_0 = Quantity with the dimension of speed (m/s)
- j = Micro-inertia density (metre²)
- D = Mass diffusivity (m^2/s)
- B_0 = Strength of the magnetic field (Web/ m^2)
- t = Time (Second)
- G_r = Grashoff number for heat transfer
- G_c = Grashoff number for mass transfer
- S_c = $\frac{\nu}{D}$, Schmidt number
- P_r = $\frac{\nu_\infty \rho c_p}{\lambda_\infty}$, Prandtl number
- R_e = $\frac{U_0 c_o}{\alpha^2 \nu_\infty}$, Reynolds number
- P_{e_h} = $P_r \cdot R_e$, Peclet number for diffusion of heat
- P_{e_m} = $S_c \cdot R_e$, Peclet number for diffusion of mass
- c_f = Skin -friction coefficient
- N_u = Nusselt number
- S_h = Sherwood number
- K_1 = $\frac{\kappa}{\nu_\infty \rho}$, Coupling constant parameter
- K_2 = $\frac{\nu_\infty \alpha}{U_0^2}$, Viscosity Parameter
- M = $\frac{\sigma B_0^2}{\rho \alpha}$, Magnetic parameter (Hartmann number)

Subscripts

- w, the condition at the wall
- ∞ , the condition at a large distance from the surface

Superscripts

- η , Differentiation with respect to η